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Cluster-Induced Deagglomeration in Dilute Gravity-Driven Gas-Solid Flows of Cohesive Grains

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1 Cluster-induced Deagglomeration in Dilute Gravity-driven Gas-solid Flows of 2 Cohesive Grains

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7 Clustering are often presumed to lead to enhanced agglomeration between cohesive grains due
8 to the reduced relative velocities of particles within a cluster. Our discrete-particle simulations on
9 gravity-driven, gas-solid flows of cohesive grains exhibit the opposite trend, revealing a new mecha-
10 nism we coin “cluster-induced deagglomeration”. Specifically, we examine relatively dilute gas-solid
11 flows, and isolate agglomerates of cohesive origin from overall heterogeneities in the system i.e., ag-
12 glomerates of cohesive origin and clusters of hydrodynamic origin. We observe enhanced clustering
13 with increasing system size (as is the norm for non-cohesive systems) as well as reduced agglomera-
14 tion. The reduced agglomeration is traced to the increased collisional impact velocities of particles
15 at the surface of a cluster i.e., higher levels of clustering lead to larger relative velocities between the
16 clustered and non-clustered regions, thereby serving as an additional source of granular temperature.
17 This physical picture is further evidenced by a theoretical model based on a balance between the
18 generation and breakage rates of agglomerates. Finally, cluster-induced deagglomeration also pro-
19 vides an explanation for a surprising saturation of agglomeration levels in gravity-driven, gas-solids
20 systems with increasing levels of cohesion, as opposed to the monotonically increasing behavior seen
21 in free-evolving or driven granular systems in the absence of gravity. Namely, higher cohesion leads
22 to more energy dissipation, which is associated with competing effects: enhanced agglomeration and
23 enhanced clustering, the latter of which results in more cluster-induced deagglomeration.

24 Due to the dissipative nature of solid-solid and fluid- 56
25 solid interactions, granular and gas-solid flows develop 57
26 hydrodynamic instabilities that lead to *clusters*: local 58
27 regions of high solid concentration [1–9], which are ab- 59
28 sent in molecular fluids. Inter-particle cohesion, such 60
29 as van der Waals force [10], liquid-bridging [11, 12] and 61
30 electrostatics [13, 14], enhances energy dissipation dur- 62
31 ing particle collisions [15, 16], causing the formation of 63
32 *agglomerates* [17, 18]. Unlike the loose collection of par- 64
33 ticles characterizing clusters, agglomerates refer to parti- 65
34 cles held together in enduring contacts by cohesion [19]. 66
35 Both clustering and agglomeration significantly impact 67
36 reaction rates, momentum, heat and mass transfer in 68
37 multiphase flows [9]. 69

38 Here, we aim to understand the interplay between clus- 70
39 ters and agglomerates. For granular systems (no fluid) 71
40 without gravity, the formation of clusters enhances ag- 72
41 glomeration. Namely, in both free-evolving [20–22] and 73
42 driven [23–25] systems, particles in clusters have higher 74
43 collision frequency due to the increased local number den- 75
44 sity. Therefore, the collisional impact velocities (relative 76
45 particle velocities prior to collisions) of particles in clus- 77
46 ters decay faster than particles in the surrounding, less 78
47 dense regions [26, 27]. With reduced impact velocities, 79
48 particles are more likely to agglomerate upon collision 80
49 [28, 29]. Moreover, the rapid energy dissipation within 81
50 clusters results in a pressure gradient across the cluster 82
51 interface which promotes the migration of free particles 83
52 towards clusters [1, 30], further increasing the cluster size 84
53 and thus the possibility of agglomeration. 85

54 In this Letter, we study the relationship between clus- 86
55 tering and agglomeration in dilute gas-solid flows of 87

lightly cohesive particles in unbounded fluidization via discrete-particle simulations. Unlike granular systems under zero gravity, gas-solid flows are driven by gravity and have two additional sources of clustering beyond dissipative particle collisions [9]: relative motion between gas and solid phases (mean drag) [4] and dissipation of granular energy due to gas viscosity (thermal drag) [3]. We report an unexpected response of agglomerates to increasing system size. Namely, analogous to fluid turbulence, the level of clustering increases with system size, as is also observed in non-cohesive systems [31]. However, unlike granular systems, the clustering in gas-solid systems does not enhance agglomeration; instead, the degree of agglomeration reduces with increased system size. This observation is surprising since particles within a cluster are characterized by reduced impact velocities, which favor enhanced agglomeration. Based on an analysis of particle velocities, we uncover the physical mechanism for this surprising behavior - *cluster-induced deagglomeration* - and establish an analytical model to predict the resulting degree of agglomeration. We then demonstrate the robustness of the mechanism at higher cohesion levels.

Following our recent work [32], unbounded fluidization [9] is simulated in a fully periodic domain with a square cross-section (Fig. 1) via coupled computational fluid dynamics and discrete element method (CFD-DEM). Compared with no-slip side walls, the periodic domain removes bulk shear in the mean flow, thereby isolating the mechanism of deagglomeration associated with clusters. In CFD-DEM, particle trajectories are integrated via Newtons equations of motion, where the contact forces

between particles are related to particle overlap [33–36]. For computational simplicity and convenient control of cohesion level, a constant cohesion is applied during physical contact of particles (i.e. “square-force” cohesion model with zero cut-off distance [37]), following previous studies [18, 38]. We recently demonstrated [37] that this square-force cohesion model is a valid surrogate of more rigorous models where cohesion may depend on interparticle separation, surface morphologies, etc. [39–44]. The gas phase governed by the Navier-Stokes equations is solved using a cell size equal to two particle diameters [45–47]. The gas and solid phases are coupled via a local, solid-concentration-dependent drag law established from direct numerical simulations [48–50]. The open-source solver MFIX [51] is used to perform the simulations. Details on the numerical method are available elsewhere [32]. In the simulations, the incompressible gas has density $\rho_g = 0.97 \text{ kg/m}^3$ and viscosity $\mu_g = 1.8335 \times 10^{-5} \text{ Pa}\cdot\text{s}$. Particles are frictionless solid spheres with diameter $d_p = 69 \times 10^{-6} \text{ m}$, density $\rho_p = 2500 \text{ kg/m}^3$, restitution coefficient $e = 0.97$, Young’s modulus $E = 10 \text{ MPa}$ and Poisson’s ratio $\nu = 0.22$. Except where noted, a cohesion force $F_c = 680 \text{ nN}$ is applied. To study the effect of system size, we vary the domain width W and height H in proportion, with constant aspect ratio $\alpha = H/W \equiv 4$ (see Fig. 3d). In simulations with W and H independently varied, flow properties show larger sensitivity to increasing W than H , which is associated with flow anisotropy (see Supplemental Materials). The overall solid concentration $\epsilon_s = 0.01$, corresponding to particle number count N_p from 2,062 to 101,680 as W varies from $30d_p$ to $110d_p$ (H from $120d_p$ to $440d_p$). Particles are initially at rest and randomly placed throughout the domain. Gas flows in the upward direction (y -direction in Fig. 1) at a constant superficial velocity $U = 43 \text{ cm/s}$. As time evolves, particles accelerate until they reach the terminal velocity, or statistical steady state. Our following analysis focuses on steady-state properties, i.e. time-averaged data over 1–4 s. (Note that varying U does not affect the steady-state gas-solid slip velocity or the levels of clustering and agglomeration, see Supplemental Materials.)

It is worth noting that the flow regime examined here corresponds to that in typical risers [4], with particle Reynolds numbers $Re_p = \rho_g d_p v_t / \mu_g = 1.3$ and mean-flow Stokes number $St_M = \rho_p d_p v_t / (9\mu_g) = 369.5$, where $v_t = \rho_p g d_p^2 / (18\mu_g)$ is the particle terminal velocity in undisturbed fluid flow [52, 53]. Therefore, fluid inertia and viscosity play a secondary role to particle inertia such that the flow, and more specifically agglomeration and breakage, is characterized by solid collisions [9, 54]. The current system therefore differs from common liquid-solid suspensions with much lower Stokes numbers ($St_M \sim O(1)$) [55–58], where deagglomeration in dilute suspensions is largely due to the solid-liquid interactions [59–67]. Examples of such low-Stokes systems

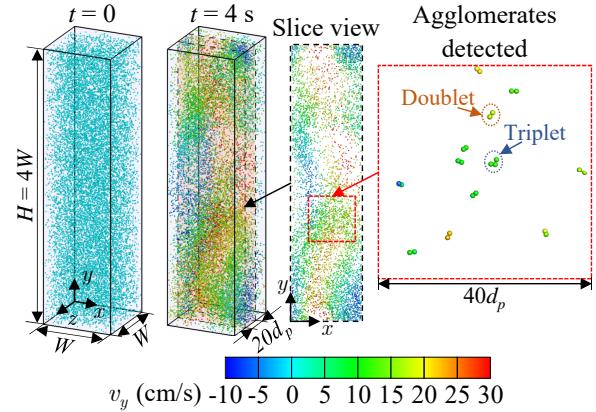


FIG. 1. Snapshots of particles at the beginning ($t = 0$) and the end ($t = 4 \text{ s}$) of the simulation with $W = 60d_p$ ($H = 240d_p$). Particles with initial random spatial distribution develop heterogeneities in particle concentration (better viewed on a $20d_p$ thick slice). The enlarged view shows the detected agglomerates from a square region marked on the slice.

are cohesive sediment transport [68, 69]. Furthermore, the effect of cluster-induced turbulence, which refers to the generation of gas-phase turbulence due to coupling with the solid phase ([31, 70, 71]), is light in our systems. Namely, the estimated ratio of turbulent viscosity associated with single-particle-induced turbulence (PIT) ν_{pit} to gas viscosity ν_{pit}/ν_g ($= 0.008$) is much smaller than unity, where $\nu_{pit} = 0.6\epsilon_s d_p v_t$ [72].

We begin our discussion with solid-phase heterogeneities, quantified by a heterogeneity index D . This index characterizes the deviation of the particle-number-density fluctuation from that corresponding to a random distribution [73]; a larger D indicates a higher level of heterogeneity. Specifically, $D = (\sigma(\epsilon_s) - \sigma_p)/\mu(\epsilon_s)$, where $\mu(\epsilon_s)$ and $\sigma(\epsilon_s)$ are the mean and standard deviation of the local number density, respectively. σ_p is the standard deviation of the Poisson distribution associated with the random distribution of particles inside the domain, and $\sigma_p = [N_p/(W^2 H)]^{1/2}$.

Fig. 2a shows the steady-state heterogeneity index $\langle D \rangle$ increases linearly with system size W . Similar trends are reported for non-cohesive particles in granular [74–76] and gas-solid flows [31, 77], where the higher level of heterogeneities in larger systems is explained by the increased space for hydrodynamic instabilities to develop [74, 78], analogous to the laminar-to-turbulent transition in single-phase pipe flows. For cohesive particles, in addition to increased clustering, an increased $\langle D \rangle$ can also result from enhanced agglomeration. However, Fig. 2b shows the levels of agglomeration decreases with W , in terms of both the steady-state fraction of particles in agglomerates $\langle A \rangle$ and the agglomerate size $\langle a \rangle$ (average number of particles in each agglomerate). To obtain A and a , we isolate agglomerates from the overall system heterogeneity by tracking enduring contacts

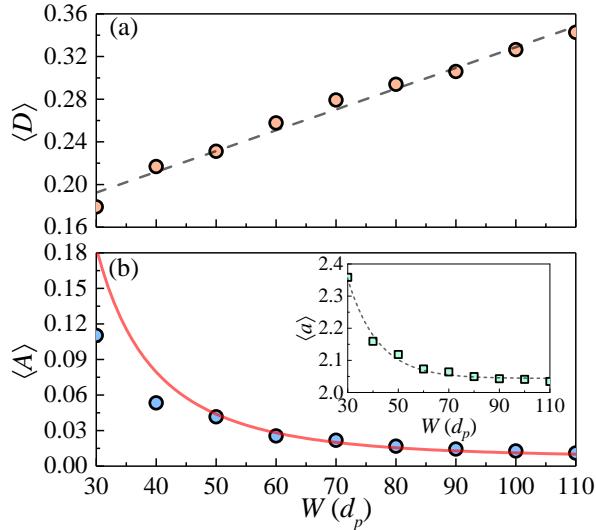


FIG. 2. Steady-state (a) heterogeneity index $\langle D \rangle$ and (b) fraction of particles in agglomerates $\langle A \rangle$ with increasing system size (W). To compute D , a cell size $l = 10d_p$ is used in extracting the local particle number density [73]. Inset for (b): steady-state mean agglomerate size $\langle a \rangle$ with increasing W . Dashed lines are linear and exponential fits for (a) and the inset of (b), respectively, to guide the eye. Solid line on (b) is Eq. (1); see text for details.

reasonable since particle-particle interactions dominate the dynamics in the transverse directions with zero mean flow ($\langle v_x \rangle, \langle v_z \rangle = 0$ on Fig. 3c). On the other hand, the streamwise distributions $f(v'_y)$ are flatter and better described by Gaussians with positive skewness, which is attributed to the stronger gas-solid interactions (larger input of granular energy [89, 90]) in the streamwise direction [71, 91–94]. As W increases, the distributions get wider in all directions. Accordingly, the steady-state granular temperatures $\langle T_i \rangle$, defined as the variances of the three components of particle fluctuating velocity [95], increase with W (Fig. 3b), consistent with gas-solid flows of non-cohesive particles [31, 93]. The increased $\langle T_i \rangle$ with system size can be traced to increased clustering. The physical picture is that clusters tend to fall down as a result of “jet-bypassing” [71]: the gas bypasses clusters, leading to reduced drag, whereas an increased pressure drop is needed for the gas to squeeze through clusters (higher flow resistance in clusters). The falling clusters then collide with individual particles or small clusters/agglomerates entrained by the gas flowing upwards. These “cluster-induced” collisions provide an added source of granular energy, which increases with the clustering level and results in higher $\langle T_i \rangle$ in larger domains. In Fig. 3d, falling clusters are increasingly visible with increasing W , i.e., more particles with lower or negative streamwise velocities v_y are seen, leading to decreased $\langle v_y \rangle$ with W (Fig. 3c).

Due to the increased $\langle T_i \rangle$, both the impact velocity and frequency of collisions increase, analogous to molecular gases at elevated thermal temperatures. Correspondingly, as shown in Fig. 4, the steady-state distributions of the normal impact velocities v_n (magnitude of the normal relative velocity right before a collision) shift to higher values with increasing W . Since agglomeration occurs at lower impact velocities [15, 29], the increased v_n is responsible for the decreasing agglomeration shown in Fig. 2b.

To explain “cluster-induced deagglomeration” with more mathematical rigor, we propose an analytical model to relate $\langle A \rangle$ to the impact velocity distribution $f(v_n)$. First, recall in current system with light cohesion, the agglomerates are largely doublets (Fig. 1). Thus, at statistical steady state, the generation and breakage rates of doublet are assumed equal, such that $\omega_{11}\psi_a = \omega_{12}\psi_b$, where ω_{11} and ω_{12} are, respectively, the frequencies of singlet-singlet and singlet-doublet collisions. ψ_a and ψ_b are, respectively, the probabilities (success factors [96]) of collisions resulting in agglomeration of singlets (from singlet-singlet collisions) and breakage of doublets (from singlet-doublet collisions). The collision frequencies $\omega_{11} = 1/2n_1^2g_0s_{11}\langle v_{rel} \rangle$ and $\omega_{12} = n_1n_2g_0s_{12}\langle v_{rel} \rangle$ [97, 98], where n_1 and n_2 are number densities of singlets and doublets, g_0 is the radial distribution function at contact, s_{11} and s_{12} are, respectively, the collisional cross section areas for singlet-singlet and singlet-

between particles. We associate particles with an agglomerate when their contact duration t_c exceeds a critical value $t_{c,crit} = 59 \times 10^{-6}$ s, considerably longer than the typical contact durations for non-agglomerating collisions [79]. Agglomerate breakage is recorded when particles lose physical contact with the agglomerate/particle. In all systems, agglomerates are dominated by doublets ($a = 2$) ($\langle a \rangle < 2.4$ on inset of Fig. 2b), consistent with Fig. 1, where we zoom in on the flow pattern at $t = 4$ s to find a few doublets and only one triplet ($a = 3$). Since agglomeration decreases as W increases, the increase in $\langle D \rangle$ with W can only be attributed to an increased clustering. Thus, in contrast to granular flows where the reduced impact velocities within clusters enhance agglomeration, clustering in gas-solid flows appears to inhibit agglomeration. To probe the mechanism for this counterintuitive behavior, the particle velocity distributions are examined next since they dictate whether or not agglomeration occurs [15, 29].

Fig. 3a shows steady-state distributions for the three components v'_i ($i = x, y, z$) of particle fluctuating velocities $\mathbf{v}' = \mathbf{v} - \bar{\mathbf{v}}$, where \mathbf{v} and $\bar{\mathbf{v}}$ are instantaneous and mean particle velocities, respectively. In transverse directions, the distributions $f(v'_x)$ and $f(v'_z)$ deviate from Gaussian (dashed lines) and exhibit overpopulated tails $\sim \exp(-|v'_i|^{3/2})$ (solid lines), which is the signature of driven, non-cohesive granular gases identified theoretically [80, 81], numerically [82, 83] and experimentally [26, 84–88]. The consistency with granular systems is

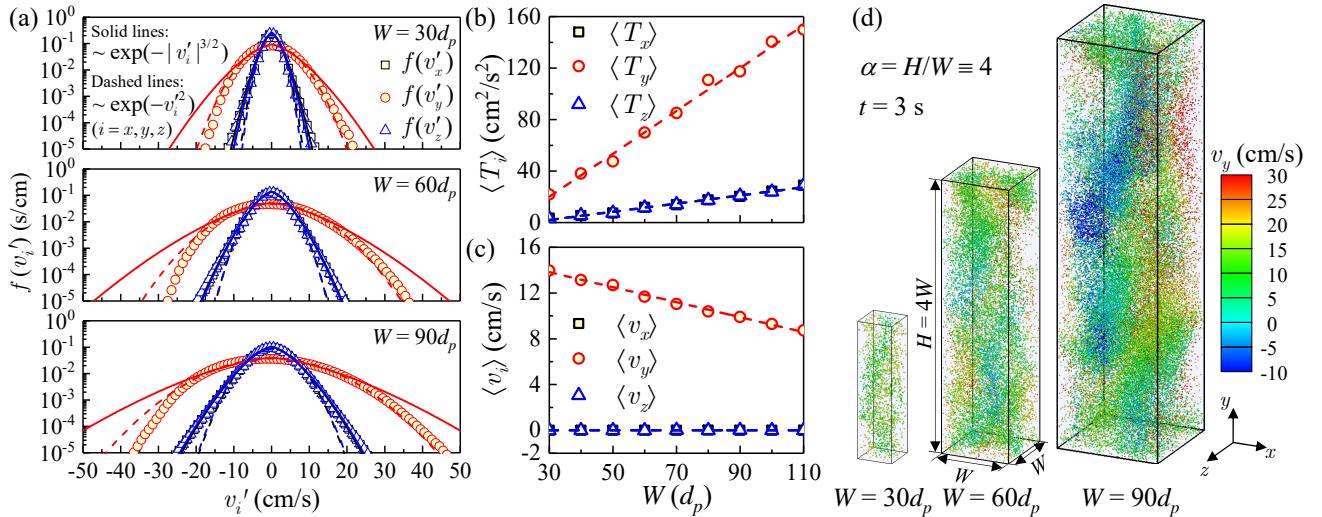


FIG. 3. (a) Steady-state distributions of particle fluctuating velocities in transverse v'_x , v'_z and streamwise v'_y directions with increasing W (symbols). Dashed lines are Gaussian $f(v'_i) = \sqrt{1/(2\pi \langle T_i \rangle)} \exp[-v'_i^2 / (2 \langle T_i \rangle)]$, ($i = x, y, z$) and solid lines are fits of $f(v'_i) = A_1 \exp[-|v'_i| / (A_2 \langle T_i \rangle)^{1/2}]^{3/2}$, where A_1 and A_2 are fitting parameters. Steady-state (b) granular temperatures $\langle T_i \rangle$ and (c) particle velocities $\langle v_i \rangle$ in three directions with increasing W . Dashed lines are linear fits to guide the eye. (d) Snapshots of particles with increasing W at $t = 3$ s. See corresponding movies in Supplemental Materials.

doublet collisions, and $\langle v_{rel} \rangle$ is the mean particle relative velocity magnitude. Since $n_1 = N_p(1 - \langle A \rangle)/V$, $n_2 = N_p \langle A \rangle / (2V)$, where V is the system volume, combining the above relations gives

$$\langle A \rangle = \left(\frac{s_{12}\psi_b}{s_{11}\psi_a} + 1 \right)^{-1}.$$

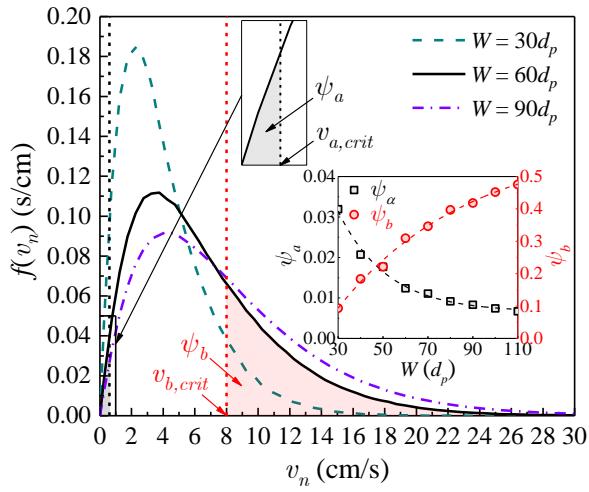


FIG. 4. Distributions of normal impact velocities v_n for collisions collected during steady states with increasing W . The vertical dashed lines mark the critical agglomeration $v_{a,crit}$ and breakage velocities $v_{b,crit}$. The shaded areas demarcate the probabilities of agglomeration (black) and breakage (red) at $W = 60d_p$. Inset: ψ_a and ψ_b with increasing W , where dashed lines are exponential fits to guide the eye.

For singlet-singlet collisions, $s_{11} = \pi d_p^2$. The singlet-doublet collisional cross section s_{12} depends on the orientation of doublets. In Supplemental Materials, we derive the average collisional cross section over possible doublet orientations in the current system, and obtain $s_{12} = 4.66d_p^2$. Next, we evaluate ψ_a and ψ_b . For singlet-singlet collisions, agglomeration occurs when v_n is below the critical agglomeration velocity $v_{a,crit}$. Using a dimensional analysis, we recently [99] derived an expression relating $v_{a,crit}$ to particle material properties: $v_{a,crit} = cF_c^{5/6}(1 - \nu^2)^{1/3}/(d_p^{5/3}\rho_p^{1/2}E^{1/3})$, where c is a dimensionless parameter dependent on particle restitution coefficient e . In this work, $e = 0.97$ and $c = 1.042$ [99], giving $v_{a,crit} = 0.6$ cm/s. In this same work [99], we conducted controlled simulations of singlet-doublet collisions for particles used here. We found the critical breakage velocity $v_{b,crit}$ (i.e. when $v_n > v_{b,crit}$, the doublet breaks and the collision results in three singlets) depends on the relative position of the singlet and doublet before colliding (pre-collisional configurations). For simplification in the current analytical model, we use $v_{b,crit} = 8.0$ cm/s, which is the averaged $v_{b,crit}$ collected in controlled simulations sweeping all possible pre-collisional configurations [99]. Therefore, we compute $\psi_a = \int_0^{v_{a,crit}} f(v_n)dv_n$ and $\psi_b = \int_{v_{b,crit}}^\infty f(v_n)dv_n$. For example, ψ_a and ψ_b corresponding to $f(v_n)$ at $W = 60d_p$ are marked on Fig. 4 as shaded areas. As W increases, $f(v_n)$ shifts towards higher values, causing ψ_a to decrease and ψ_b to increase (inset of Fig. 4). Plugging s_{11} , s_{12} , ψ_a and ψ_b in Eq. (1), we find the decreasing $\langle A \rangle$ with increasing W is well captured by Eq. (1) (solid line on Fig. 2b). Quantitative agreement is observed except at

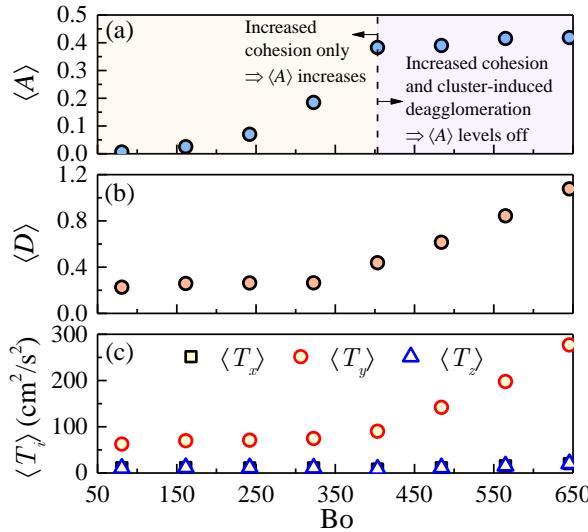


FIG. 5. Steady-state (a) agglomerate fraction $\langle A \rangle$, (b) heterogeneity index $\langle D \rangle$ and (c) granular temperatures $\langle T_i \rangle$ as a function of granular bond number $Bo = F_c/mg$ under $W \equiv 60d_p$ ($H \equiv 240d_p$).

uration of agglomeration levels as cohesion increases in gravity-driven gas-solid flows. Therefore, it is the gravity and the resulting increased collisional velocities between the falling (large) clusters and rising particles or (small) clusters that leads to the cluster-induced deagglomeration. Collectively, such interplay between clusters and agglomerates will impact numerous multiphase operations, where the interphase drag, heat transfer and chemical reactions rates are dependent on the nature of particle contacts (brief in clusters vs. enduring in agglomerates, etc.) [100–103]. The identification of the cluster-induced deagglomeration warrants its consideration in related population balance efforts [21, 79, 104, 105] for developing continuum models of cohesive particles. Beyond gas-solid flows, the findings may have ramifications for (high Stokes number) gravity-driven liquid-solid suspensions [106], colloids [107], emulsions and foams [108], where hydrodynamic instabilities and long-range interparticle attractions coexist.

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