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Phys. Rev. Fluids **2**, 092601 — Published 21 September 2017

DOI: [10.1103/PhysRevFluids.2.092601](https://doi.org/10.1103/PhysRevFluids.2.092601)

Integral Analysis of Boundary Layer Flows with Pressure Gradient

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(Dated: September 11, 2017)

Abstract

This paper investigates boundary layer flows with pressure gradient using a novel similarity/integral analysis of the continuity equation and momentum equation in the streamwise direction. The analysis yields useful analytical relations for V_e , the mean wall-normal velocity at the edge of the boundary layer, and for the skin friction coefficient, C_f , in terms of the boundary layer parameters and in particular β_{RC} , the Rotta-Clauser pressure gradient parameter. The analytical results are compared with experimental and numerical data and are found to be valid. One of the main findings is that for large positive β_{RC} (important effect of an adverse pressure gradient), the friction coefficient is closely related to β_{RC} as $C_f \propto 1/\beta_{RC}$, because δ/δ_1 , $\delta_1/\delta_2 = H$ and $d\delta/dx$ become approximately constant. Here δ is the boundary layer thickness, δ_1 is the displacement thickness, δ_2 is the momentum thickness and H is the shape factor. Another finding is that the mean wall-normal velocity at the edge of the boundary layer is related to other flow variables as $U_e V_e / u_\tau^2 = H + (1 + \delta/\delta_1 + H)\beta_{RC}$, where U_e is the streamwise velocity at the edge of the boundary layer. At zero pressure gradient, this relation reduces to $U_\infty V_\infty / u_\tau^2 = H$ as recently derived by Wei and Klewicki[1].

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20 I. INTRODUCTION

21 Turbulent boundary layer flows subject to pressure gradient occur in many engineering
22 applications, for example diffusers, turbine blades, trailing edges of airfoils and the aft section
23 of ship hulls. In particular, turbulent boundary layer flows with adverse pressure gradient
24 (APG) often play a critical role in determining the performance of engineering devices.
25 Under strong APG the boundary layer flow may separate from the solid surface, causing a
26 drastic change to the flow pattern. In many occasions, accurate knowledge of the adverse
27 pressure gradient boundary layer development is the most critical factor in predicting the
28 overall performance of the device.

29 Due to its significance, the APG TBL has been the subject of numerous theoretical,
30 experimental and numerical studies over the past six decades. The idea behind the equilib-
31 rium turbulent boundary layer was laid out by Rotta [2] and by Clauser [3], who examined
32 a boundary layer with a well defined and simple pressure history. Clauser defined an equi-
33 librium profile as one of a set of profiles in which a constant force history is obtained. In his
34 analysis Clauser introduced a non-dimensional pressure gradient parameter β_{RC} , commonly
35 called Rotta-Clauser parameter:

$$\beta_{RC} = \frac{\delta_1}{u_\tau^2} \frac{1}{\rho} \frac{dP}{dx} = -\frac{\delta_1}{u_\tau^2} U_e \frac{dU_e}{dx}, \quad (1)$$

36 where δ_1 is the displacement thickness of the boundary layer, $u_\tau = \sqrt{\tau_w/\rho}$ is the friction
37 velocity and U_e is the free stream velocity.

38 Following Rotta and Clauser, during the last six decades numerous researchers have stud-
39 ied the APG TBL, analytically, experimentally and numerically, e.g., [4–14]. Our knowledge
40 and understanding of boundary layer flows with pressure gradient are, however, still incom-
41 plete.

42 The goal of the present study is to use integral and similarity analysis to gain a better
43 understanding of the relationship between important parameters of PG TBLs. The relation-
44 ships analytically developed herein are useful for the physical understanding of such flows,
45 and to estimate important flow parameters. Integral analysis of the boundary layer equa-
46 tions is almost as old as boundary layer theory itself (Pohlhausen 1921[15], von Kármán
47 1921[16]). In the case of turbulent boundary layers, it has led to a panoply of integral
48 methods that continue to be used in engineering analysis. It is important to stress that the

49 present similarity/integral analysis was not, however, performed to design a new integral
 50 method to compute turbulent boundary layers or to obtain closure relationships for integral
 51 methods. Rather, the novelty of the present integral analysis is twofold. The first relates
 52 to the manner in which the integral continuity and momentum equations are combined.
 53 The second is that the integral equations are expressed in terms of the pressure gradient
 54 parameter. This is convenient and useful because of the importance of this parameter in
 55 describing PG flows.

56 One of the unique objectives of the present study is to investigate how the mean wall-
 57 normal velocity at the edge of APG TBLs, V_e , evolves under the action of a pressure gradient.
 58 In the traditional integral analysis, the mean wall-normal velocity is not explicitly utilized.
 59 In fact, due to its small magnitude, the mean wall-normal velocity has been largely ignored
 60 in previous studies of turbulent boundary layer flows. In ZPG boundary layer flows, the
 61 mean wall-normal velocity monotonically increases from 0 at the surface to a maximum
 62 value outside the boundary layer as sketched in figure 1. However, in boundary layer flows
 63 with APG, the mean wall-normal velocity continues to increase outside the boundary layer
 64 as also illustrated in figure 1.

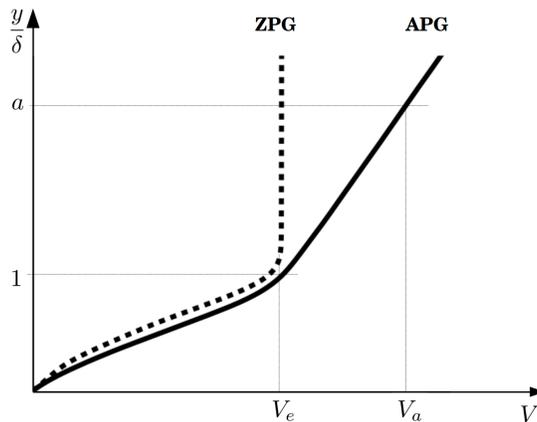


FIG. 1. Sketch illustrating the shape of the mean wall-normal velocity in boundary layer flows with
 zero-pressure-gradient (ZPG) or adverse-pressure-gradient (APG).

67 We start the analysis by assuming self-similarity of the velocity moments in the continuity
 68 equation and the streamwise mean momentum balance equation. Subsequent integration of
 69 both equations from the surface at $y = 0$ to outside the boundary at $y = a\delta$ (see Fig.
 70 1) yields relationships for V_e and C_f in terms of the boundary layer parameters, and in

71 particular in terms of β_{RC} . Experimental and numerical data are compared with these
 72 analytical relations, and the overall agreement is assessed.

73 II. SIMILARITY/INTEGRAL ANALYSIS

74 This work considers two-dimensional boundary layer flows in which the mean flow only
 75 varies in the streamwise x and wall-normal y directions, and is statistically homogeneous in
 76 the spanwise direction z . The governing equations for the 2D boundary layer flows, i.e., the
 77 continuity equation and mean momentum balance equation in the streamwise direction, are

$$\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} = 0, \quad (2)$$

$$U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} - \nu \frac{\partial^2 U}{\partial y^2} - \frac{\partial T}{\partial y} + \frac{1}{\rho} \frac{dP}{dx} = 0, \quad (3)$$

78 where $T = -\langle u'v' \rangle$ is the kinematic Reynolds shear stress. (Note that the contribution
 79 of $\partial \langle u'u' \rangle / \partial x$ is neglected in the present analysis. Near separation and for strongly accel-
 80 erated/decelerated flows, such an assumption might not be adequate.) Setting T to zero
 81 results in the equation for laminar boundary layer flows. As the Reynolds shear stress is
 82 zero at the wall and outside the boundary layer, the present analysis also applies to laminar
 83 boundary layers with pressure gradient.

84 The only assumption in the following development is that the boundary layer is assumed
 85 to be self-similar. This is of course not the case for many PG flows since they are often not
 86 in dynamic equilibrium. Imposing self-similarity of the velocity moments is equivalent to
 87 assuming that the TBL is in a state of quasi-equilibrium. The next section will demonstrate
 88 under what conditions this assumption can be considered to approximately hold.

89 In this work, the boundary layer thickness δ and the streamwise velocity U_e at the edge of
 90 the boundary layer are used to normalize the flow variables. The normalized flow variables
 91 are

$$U^*(\eta) \equiv \frac{U(x, y)}{U_e(x)}; \quad V^*(x/\delta, \eta) \equiv \frac{V(x, y)}{U_e(x)}; \quad T^*(x/\delta, \eta) \equiv \frac{T(x, y)}{U_e^2(x)}; \quad \eta \equiv \frac{y}{\delta(x)}. \quad (4)$$

92 Assuming self-similarity for U^* (V^* and T^* do not need to be assumed self-similar as
 93 the equations do not involve $\partial V / \partial x$ or $\partial T / \partial x$), the normalized derivatives appearing in the
 94 governing equations are as listed in table I. Note that the assumed self-similarity $U^*(\eta)$
 95 does not contradict the classical self-similarity assumption [2, 3]: $(U_e - U) / u_\tau = \hat{U}(\eta)$.

96 Self-similarity of the TBL requires $u_\tau/U_e = \text{constant}$ [5, 11]. It follows that $U/u_\tau = f(\eta)$
 97 and hence $U/U_e = U^*(\eta)$. Consequently, the present analysis recasts the continuity and
 98 momentum equations in different forms than in the classical similarity analysis, but it does
 99 not contradict it in any manner.

$\frac{\partial U}{\partial x} = -\frac{U_e}{\delta} \frac{d\delta}{dx} \eta \frac{\partial U^*}{\partial \eta} + \frac{dU_e}{dx} U^*$,	$\frac{\partial U}{\partial y} = \frac{U_e}{\delta} \frac{\partial U^*}{\partial \eta}$,	$\frac{\partial^2 U}{\partial y^2} = \frac{U_e}{\delta^2} \frac{\partial^2 U^*}{\partial \eta^2}$.
$\frac{\partial V}{\partial y} = \frac{U_e}{\delta} \frac{\partial V^*}{\partial \eta}$,	$\frac{\partial T}{\partial y} = \frac{U_e^2}{\delta} \frac{\partial T^*}{\partial \eta}$.	

TABLE I. Normalized derivatives in the governing equations.

100 Substituting the normalized derivatives, the non-dimensional continuity equation be-
 101 comes

$$\frac{\partial V^*}{\partial \eta} = \frac{d\delta}{dx} \eta \frac{\partial U^*}{\partial \eta} - \frac{\delta}{U_e} \frac{dU_e}{dx} U^*. \quad (5)$$

102 Integrating this equation from the surface $\eta = 0$ to outside the boundary layer $\eta = a$ (where
 103 $a \geq 1$) yields

$$\frac{V_a}{U_e} = \frac{d\delta}{dx} \frac{\delta_1}{\delta} + \frac{u_\tau^2}{U_e^2} \left(a \frac{\delta}{\delta_1} - 1 \right) \beta_{RC}. \quad (6)$$

104 Multiplying U_e^2/u_τ^2 on both sides of equation 6 yields

$$\frac{U_e V_a}{u_\tau^2} = \frac{\delta_1}{\delta} \frac{d\delta}{dx} \frac{U_e^2}{u_\tau^2} + \left(a \frac{\delta}{\delta_1} - 1 \right) \beta_{RC}. \quad (7)$$

105 In many previous experiments, V is not measured. However, if $d\delta/dx$ can be extracted from
 106 measurements, equation 7 can be used to calculate $U_e V_a/u_\tau^2$, indirectly.

107 Substituting the normalized variables, the non-dimensional mean momentum equation in
 108 the streamwise direction becomes

$$-U^* \frac{\partial V^*}{\partial \eta} + V^* \frac{\partial U^*}{\partial \eta} - \frac{\nu}{\delta U_e} \frac{\partial^2 U^*}{\partial \eta^2} - \frac{\partial T^*}{\partial \eta} + \frac{\delta}{\delta_1} \frac{u_\tau^2}{U_e^2} \beta_{RC} = 0. \quad (8)$$

109 Replacing $\partial V^*/\partial \eta$ from the continuity equation 5, and integrating equation 8 from $\eta = 0$ to
 110 $\eta = a$ yields

$$-\frac{d\delta}{dx} \left(\frac{\delta_1}{\delta} + \frac{\delta_2}{\delta} \right) - 2 \frac{\delta}{\delta_1} \left(a - \frac{\delta_1}{\delta} - \frac{\delta_2}{\delta} \right) \frac{u_\tau^2}{U_e^2} \beta_{RC} + \frac{V_a}{U_e} + \frac{u_\tau^2}{U_e^2} + a \frac{\delta}{\delta_1} \frac{u_\tau^2}{U_e^2} \beta_{RC} = 0. \quad (9)$$

111 Combining equations 6 and 9 yields a relation for V_a

$$\frac{U_e V_a}{u_\tau^2} = H + \left(1 + a \frac{\delta}{\delta_1} + \frac{\delta_1}{\delta_2} \right) \beta_{RC}, \quad (10)$$

112 or

$$U_e V_a = H u_\tau^2 + \left(1 + a \frac{\delta}{\delta_1} + \frac{\delta_1}{\delta_2}\right) \delta_1 \frac{1}{\rho} \frac{dP}{dx}. \quad (11)$$

113 At separation $u_\tau = 0$, and thus

$$U_e V_a = \left(1 + a \frac{\delta}{\delta_1} + \frac{\delta_1}{\delta_2}\right) \delta_1 \frac{1}{\rho} \frac{dP}{dx}, \quad \text{or} \quad V_a = - \left(1 + a \frac{\delta}{\delta_1} + \frac{\delta_1}{\delta_2}\right) \delta_1 \frac{dU_e}{dx}. \quad (12)$$

114 Setting $a = 1$ in the above relations produces the scaling for the mean wall-normal velocity
115 at the edge of the boundary layer, V_e .

116 For zero-pressure gradient boundary layer flows where $\beta_{RC} = 0$, equation 10 recovers the
117 relation derived by Wei and Klewicki[1]

$$\frac{U_\infty V_\infty}{u_\tau^2} = H. \quad (13)$$

118 Equating the right hand sides of equations 7 and 10 yields

$$C_f = \frac{2 \frac{\delta_1}{\delta} \frac{d\delta}{dx}}{H + (2 + H) \beta_{RC}}. \quad (14)$$

119 For $\beta_{RC} \gg 1$, the experimental and numerical data below indicate that $\delta_1/\delta \approx 0.5$, $H =$
120 $\delta_1/\delta_2 \approx 3 - 4$ and $d\delta/dx \approx 0.08 - 0.24$. Thus, at large β_{RC} the friction coefficient can be
121 approximated by

$$C_f \approx \frac{2 \frac{\delta_1}{\delta} \frac{d\delta}{dx}}{2 + H} \frac{1}{\beta_{RC}} \approx \frac{0.01 \sim 0.03}{\beta_{RC}}. \quad (15)$$

122 To our knowledge, the above analytical relations are new. Before comparing them with
123 data, a few remarks are warranted. First, it should be noted that C_f and β_{RC} are also linked
124 by virtue of their definitions (see eq. 1):

$$C_f = - \frac{2 \delta_1}{U_e} \frac{dU_e}{dx} \frac{1}{\beta_{RC}}. \quad (16)$$

125 However, in this case the external flow parameters, namely the external velocity and its
126 streamwise derivative, appear explicitly. In contrast, equation 14 solely involves parameters
127 that are directly related to the structure of the boundary layer. Arguably, these parameters
128 better reflect the state of the boundary layer, since the boundary layer does not respond
129 instantly to pressure gradient variations. Consequently, we are able to obtain the approxi-
130 mation at large β_{RC} given by equation 15.

131 It is also interesting to observe that the approximations that led to equation 15 can be
132 linked to the similarity analyses of turbulent boundary layers as developed by Rotta[2, 5]

133 and Maciel et al.[11]. In the latter analyses, self-similarity implies that

$$\frac{d\delta}{dx} = const, \quad H = const, \quad \frac{\delta_1}{\delta} = const. \quad (17)$$

134 To our knowledge, equilibrium TBLs represent the only case where these parameters are
135 known to be constant.

136 Self-similarity also implies

$$\Lambda = -\frac{\delta}{U_e} \left(\frac{d\delta}{dx} \right)^{-1} \frac{dU_e}{dx} = const. \quad (18)$$

137 Combining equations 16 and 18 yields a relation for C_f similar to equation 15,

$$C_f = \Lambda \frac{2\delta_1}{\delta} \frac{d\delta}{dx} \frac{1}{\beta_{RC}}. \quad (19)$$

138 Comparison of equations 15 and 19 results in a relation for self-similar TBLs at large β_{RC}

$$\Lambda \approx \frac{1}{2+H} \approx 0.17 \sim 0.25. \quad (20)$$

139 In equation 20 it is assumed that $2 \leq H \leq 4$. This range of values of Λ indeed corresponds
140 to the values usually found in the case of large-defect self-similar TBLs [11].

141 Finally, combining equations 14 and 19 yields an exact relation valid for all self-similar
142 TBLs

$$\Lambda = \frac{\beta_{RC}}{H + (2+H)\beta_{RC}}. \quad (21)$$

143 Note that a relation equivalent to equation 21 has been obtained by Rotta [5], but with
144 $u_\tau/U_e * G$ instead of H , and Δ instead of δ . Skote, Henningson and Henkes [17] presented
145 the relation with δ_1 instead of δ .

146 III. COMPARISONS WITH NUMERICAL AND EXPERIMENTAL DATA

147 The analytical relations developed are now compared with experimental and numerical
148 simulation data of APG TBLs. Experiments include those by Angele and Muhammad-
149 Klingmann (AM)[12], Indinger [9], Knopp et al.[18], Maciel et al.[11], Marusic and Perry
150 (MP)[10], Shafiei Mayam[19] and Skare and Krogstad (SK)[20]. In the case of numerical
151 simulations, we use the DNS data of Gungor et al. (GMSS)[21], Skote and Henningson
152 (SH)[22], Spalart and Watmuff (SW)[23], and the LES data of Hickel [13]. All these flows
153 are non-equilibrium TBLs whose mean velocity defect increases in the streamwise direction.

154 In the case of Skare and Krogstad [20], the last seven streamwise positions out of twelve are
 155 in a zone of near equilibrium, with almost self-similar mean velocity and Reynolds stress
 156 profiles. Hickel’s LES [13] is an attempt to numerically reproduce the flow case of Indinger
 157 [9]. These two flows are therefore similar and represent a strongly decelerated situation with
 158 massive separation downstream. The other flows constitute different dynamical evolutions
 159 of the mean momentum balance.

160 Since δ/δ_1 , H , and $d\delta/dx$ are the parameters in the derived relations for V_e and C_f ,
 161 we first present experimental and numerical data of these parameters as a function of β_{RC} .
 162 Figure 2 shows that, as expected, (1) $\frac{\delta}{\delta_1}$ decreases, monotonically, from a value of about
 163 10 to about 2 at very large β_{RC} , and (2) H increases, monotonically, from a value of about
 164 1.3 – 1.4 to about 3.5 – 4. An interesting point is that both $\frac{\delta}{\delta_1}$ and H vary slowly with β_{RC}
 165 for $\beta_{RC} > 100$. Moreover, their variations lead to $S = 1 + \frac{\delta}{\delta_1} + H \approx 6$ for $\beta_{RC} > 10$. S
 166 appears in equation 10 for V_e (setting $a = 1$).

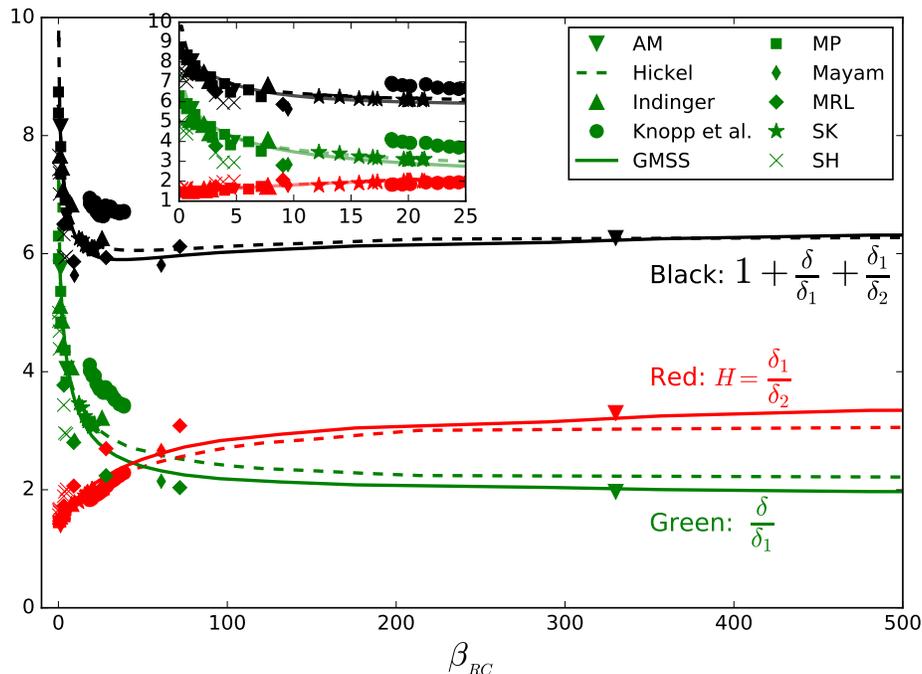


FIG. 2. Ratio of boundary layer thicknesses. See text for references.

167 With the exception of the last seven streamwise positions of SK [20] (the ones with
 168 $\beta_{RC} \approx 20$), all the other flows and flow zones are not in equilibrium. Thus, for these cases it
 169 is not surprising that $\frac{\delta}{\delta_1}$ and H evolve differently with β_{RC} from one flow to another, as these
 170 flows are subject to different upstream history effects[24]. Moreover, the differences between

171 APG TBLs can be accentuated by Reynolds number effects since the Reynolds number is
 172 relatively low for some databases, e.g., the DNS of SH [22] where $Re_\tau \approx 100$. Finally, it
 173 is worth pointing out that in most experiments the integral length scales, δ_1 and δ_2 , can
 174 usually be obtained accurately while the uncertainty of δ is much larger[25].

175 Figure 3 shows the dependence of the boundary layer growth rate $d\delta/dx$ on β_{RC} . Central
 176 finite difference was used to calculate $d\delta/dx$. In many experiments, the distance between
 177 x -stations is not small, so it is unavoidable that the calculated $d\delta/dx$ has fairly high un-
 178 certainty. Nonetheless, it is reasonable to state that at sufficiently large β_{RC} , $d\delta/dx$ varies
 179 slowly with β_{RC} . It becomes nearly constant with values in the range 0.08 – 0.24. More
 180 data are, however, needed to verify this. The different values of $d\delta/dx$ for a given β_{RC}
 181 are expected since $d\delta/dx$ is strongly dependent on the upstream and local strength of the
 182 deceleration/acceleration, as well as the Reynolds number.

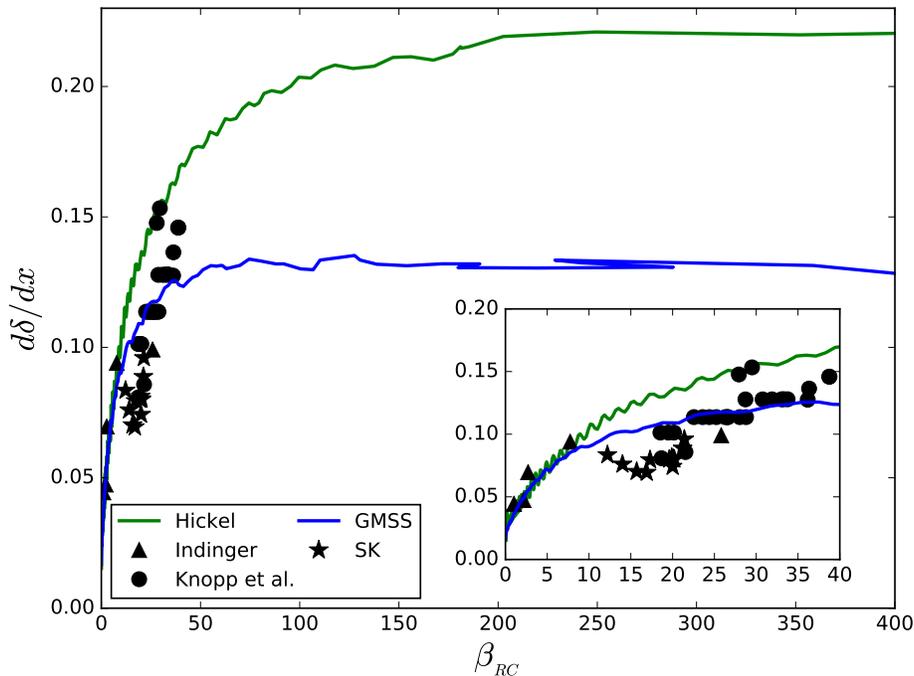


FIG. 3. Growth rate of boundary layer thickness, $d\delta/dx$, as a function of β_{RC} .

183 Figure 4 plots experimentally and numerically determined skin friction coefficient data for
 184 varying β_{RC} . The various flows follow different trends of decreasing C_f with β_{RC} . Again, this
 185 is expected because of the different streamwise evolutions of these non-equilibrium TBLs,
 186 and because of their different Reynolds numbers. Nonetheless, figure 4a shows that the data
 187 agree well with the approximate trend predicted by equation 15 for large β_{RC} . It should be

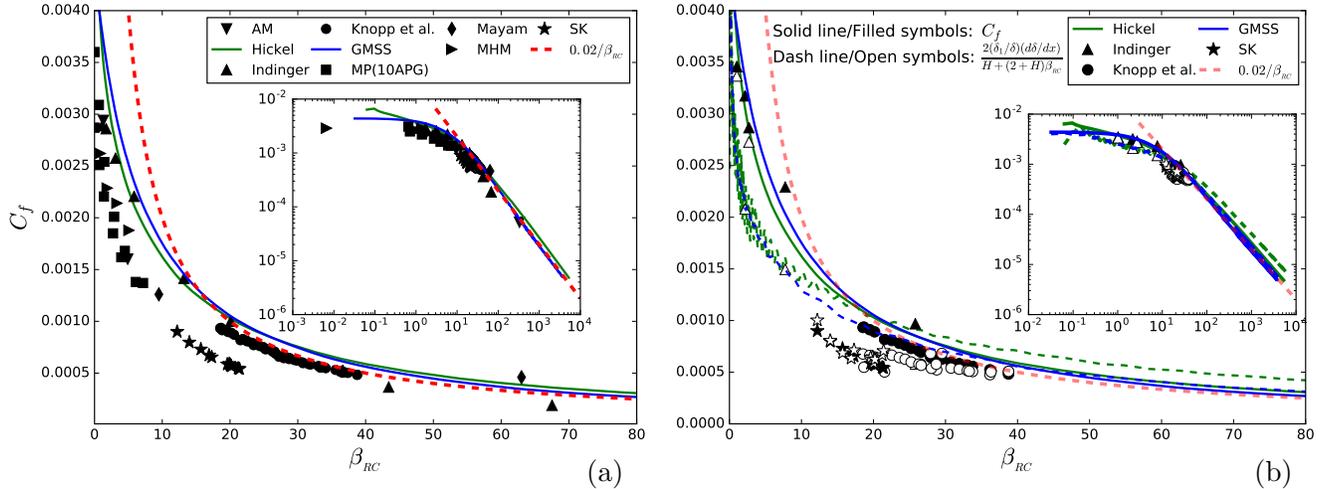


FIG. 4. (a) Skin friction coefficient in APG TBLs as a function of β_{RC} . (b) Compare analytical relation 14, $C_f = \frac{2\frac{\delta_1}{\delta} \frac{d\delta}{dx}}{H+(2+H)\beta_{RC}}$, with experimental and numerical data.

188 noted that experiments with values of β_{RC} larger than 50 are rare. They include AM [12],
 189 Indinger [9] and, for the same flow, Maciel et al.[26] and Shafiei Mayam [19]. The DNS of
 190 GMSS [21] and the LES of Hickel [13] cover a wider range of β_{RC} , including a region with a
 191 separation bubble.

192 The left and right hand sides of equation 14 are compared in figure 4b for data sets that
 193 allow $d\delta/dx$ to be reasonably estimated. Not surprisingly, equation 14, which assumes self-
 194 similarity, works essentially perfectly for SK flow (open and filled symbols overlap) since it is
 195 in quasi-equilibrium. However, even in the case of the four other flows that are all in strong
 196 disequilibrium, both sides of the equation follow similar trends. Equation 14 is therefore
 197 seen to be a reasonable approximate relation between C_f and β_{RC} even for non-equilibrium
 198 TBLs, at least in the case of a decelerating U_e .

199 The left and right hand sides of equations 7 and 10 are compared with numerical and
 200 experimental data in figure 5. Experimental data of V for APG TBLs are very rare due to
 201 the challenges involved in its measurement. Maciel and collaborators have measured V in
 202 the case of a strongly decelerated TBL covering a wide range of β_{RC} [19, 26]. In compari-
 203 son, numerical simulations provide detailed data on all velocity components, including V .
 204 However, numerical simulations are in general limited to low to moderate Reynolds numbers.

205 Figure 5 shows that $U_e V_e / u_\tau^2$ and the right hand sides of equations 7 and 10 grow approx-
 206 imately linearly with β_{RC} , even for the cases having $\beta_{RC} < 10$. Yet, in the latter cases, $\frac{\delta}{\delta_1}$,

207 H and $d\delta/dx$ vary greatly with β_{RC} . The only exception to this near linear growth occurs
 208 for the LES data of Hickel with $U_e V_e / u_\tau^2$ (green line) and the right hand side of equation 7
 209 (dash-dot green line). An explanation has not yet been found for these different behaviors.
 210 The smaller differences between $U_e V_e / u_\tau^2$ and the right hand sides of equations 7 and 10 may
 211 be due to the difficulties in obtaining accurate estimates of δ and, in the case of experiments,
 212 to measurement uncertainties of V_e , u_τ and β_{RC} .

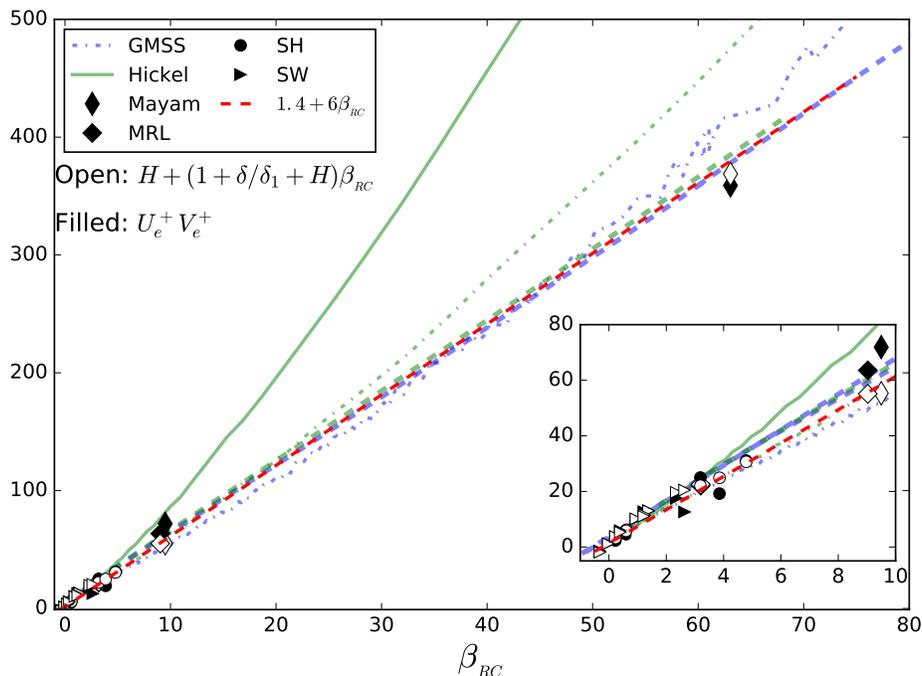


FIG. 5. Comparing analytical relations 7 and 10 with numerical and experimental data. Filled symbols and solid lines: $U_e V_e / u_\tau^2$; Open symbols and dash lines: $H + (1 + \delta/\delta_1 + H)\beta_{RC}$. Dash-dot lines: right hand side of equation 7; Red dash line: $1.4 + 6\beta_{RC}$. See text for references.

213 IV. CONCLUSION

214 In this work, APG flows are investigated using a new similarity/integral analysis of the
 215 continuity and mean momentum equations. Analytical relations are derived for the mean
 216 wall-normal velocity at the edge of the boundary layer and for the skin friction coefficient.
 217 This approach allows one to determine how these parameters evolve with the Rotta-Clauser
 218 pressure gradient parameter. To the authors knowledge, these analytical relations are new.
 219 The equation relating skin friction to the Rotta-Clauser pressure gradient parameter is of

particular interest. Specifically, the analysis yields an equation that indicates how structural parameters of the boundary layer affect the dependence of skin friction on the Rotta-Clauser pressure gradient parameter. Although the equation is only approximate for non-equilibrium flows, we have shown that the trends are nonetheless well captured by it in the case of decelerating turbulent boundary layers. Furthermore, thanks to this new analytical relation, a simple approximate relation is found between the skin friction coefficient and the Rotta-Clauser parameter for large values of the latter. New relations for self-similar turbulent boundary layers are developed. These explain, for example, the non-dimensional growth rates usually found in experiments at large β_{RC} . Finally, the new relation for the mean wall-normal velocity is of interest since pressure gradients (especially adverse) rather strongly modify boundary layer growth.

Like all other theoretical analyses of PG TBLs, the present analysis assumes local dynamic equilibrium of the flow. Thus, the relations developed cannot account for upstream effects of the pressure gradient, curvature and transition. Not surprisingly, the results presented in this paper suggest that ratios of boundary layer thicknesses, boundary layer growth and skin friction are affected by upstream history effects, at least for moderate values of the pressure gradient parameter. Upstream history effects cannot, however, be isolated from Reynolds number effects with the datasets available in the literature. An important contribution would be to design and conduct future experiments capable of isolating these effects.

V. ACKNOWLEDGMENT

The authors thank Dr. Hickel and Dr. Knopp for generously sharing their data. The financial support of New Mexico Institute of Mining and Technology and Los Alamos National Laboratory (LANL-399931) is gratefully acknowledged by T. W. Y. M. thanks NSERC of Canada for its financial support.

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