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Mass flow through solid ^4He induced by the fountain effect

M.W. Ray and R.B. Hallock

*Laboratory for Low Temperature Physics, Department of Physics,
University of Massachusetts, Amherst, MA 01003*

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Using an apparatus that allows superfluid liquid ^4He to be in contact with hcp solid ^4He at pressures greater than the bulk melting pressure of the solid, we have performed experiments that show evidence for ^4He mass flux through the solid and the likely presence of superfluid inside the solid. We present results that show that a thermomechanical equilibrium in quantitative agreement with the fountain effect exists between two liquid reservoirs connected to each other through two superfluid-filled Vycor rods in series with a chamber filled with solid ^4He . We use the thermomechanical effect to induce flow through the solid and measure the flow rate. On cooling, mass flux appears near $T = 600$ mK and rises smoothly as the temperature is lowered. Near $T = 75$ mK a sharp drop in the flux is present. The flux increases as the temperature is reduced below 75 mK. We comment on possible causes of this flux minimum.

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I. INTRODUCTION

In 2004, Kim and Chan¹ observed a decrease in the resonant period of a torsional oscillator filled with solid ^4He , which they interpreted as likely evidence for a superfluid phase of solid helium. This observation stimulated renewed interest in the low temperature properties of solid ^4He . Aside from the torsional oscillator experiments, which have been replicated in several different laboratories (for recent reviews see references [2–4]), unexpected behavior has also been observed in the shear modulus of solid helium where the solid helium is seen to become stiffer at the same temperature at which the torsional oscillator experiments show a decrease in the resonant period⁵. Further, the shear modulus increase shows the same dependence on ^3He concentration and temperature as the period shift of the torsional oscillators, which suggests that there is a connection between the results of the torsional oscillator and shear modulus experiments. This connection has been emphasized recently⁶. A peak in the heat capacity⁷ of solid helium was also observed, which may indicate that a phase transition takes place in the solid.

It is unlikely that these observations support a “supersolid”⁸ phase of the type originally proposed by the early theoretical studies^{9–11}, which were based on the presence of vacancies. In fact, the possibility that delocalized vacancies form a superfluid in solid helium at very low temperature has been recently shown by theorists to be impossible^{12–15}. Torsional oscillator measurements made on quench-cooled, highly disordered crystals show a large period shift, while in annealed crystals the effect nearly disappears¹⁶. Such behavior points to a disorder-driven phenomenon, meaning that the period shift may not be an intrinsic property of the solid. In fact, some defects, such as grain boundaries¹⁷ and dislocations¹⁸ have been shown in simulations to support a superfluid phase, as has glassy, or amorphous, solid helium^{19,20}. The observed heat capacity peak⁷ may also be explained by a

glass transition²¹. This glass transition theory, which does not invoke the presence of a superfluid phase, is supported by experimental data showing a T^2 contribution to the pressure of solid helium as a function of temperature²², as well as the observations of long time constants at lower temperatures²³, both of which can be explained by glassy regions in the solid^{21,24}.

Adding to the complexity of the situation is a torsional oscillator experiment²⁵ that shows disorder may affect the high temperature properties of the solid but not the low temperature properties. This is consistent with what is observed for the shear modulus, which shows stiffening at low temperatures, but where stressing and annealing the solid affect the high temperature properties of the solid²⁶. These measurements lead to the interpretation that there may be no evidence for supersolid behavior in torsional oscillator measurements. Rather, it has been suggested that there is elasticity at higher temperatures and as the temperature is lowered elasticity is reduced, which causes the period of solid-filled torsional oscillators to decrease. Softening of solid ^4He has also been seen recently by acoustical techniques and interpreted as consistent with the unbinding of dislocations from ^3He impurities²⁷.

On the other hand, some experiments seem to support the supersolid interpretation. Recent, simultaneous torsional oscillator and shear modulus measurements appear to show a suppression of the resonant period drop of the torsional oscillator under D.C. rotation²⁸, with no rotation effect on the shear modulus measurements on the solid in a different location in the same apparatus. These simultaneous measurements made under rotation have been interpreted²⁸ as evidence for the existence of a superfluid phase in the solid. Other experiments that may provide evidence for a supersolid phase are (1) the torsional oscillator experiments that used Vycor¹ or porous gold²⁹, which seem hard to explain by the presence of dislocations, and (2) the reduced signal seen in a blocked-annulus experiment³⁰. However, a different blocked an-

nulus experiment by Rittner and Reppy, unpublished but noted in ref [31], provided results that complicate the picture.

If solid helium does indeed support superfluidity, then it should be possible to induce mass flow in solid helium and one would expect to find a flow-limiting critical velocity. Such a flow has been seen by injecting mass into one side of the solid, and observing a pressure relaxation in a reservoir on the other side^{32,33} for $T \lesssim 550$ mK. The mass flux was seen to be independent of the driving pressure difference, which is consistent with a superflow at critical velocity. Frost heave³⁴, plastic flow, or liquid channels³⁵⁻³⁷ that might provide alternate explanations for the data that show mass flux through the solid seem inconsistent with the behavior of the flux as a function of pressure and temperature. Those flow experiments were different in various respects from other flow experiments³⁸⁻⁴³ in that they were simultaneously (1) performed at pressures greater than the bulk melting pressure, and (2) done by injecting mass into the solid, and not by trying to push bulk solid through a constrained geometry. Experiments which have attempted to mechanically push solid ^4He through small-dimensioned passages have never shown any mass flow^{39-41,43}; squeezing the lattice directly does not result in mass flow.

Here we use an apparatus similar to that used in our previous flow experiments^{32,33}, which allows us to have superfluid liquid helium in contact with the solid at a pressure greater than the bulk melting pressure of solid helium. We present two main results, which were briefly reported on previously^{44,45}, that support the possibility that superfluidity exists in solid helium. In section II we describe the concept of the experiments and describe in detail the apparatus used. In section III we present results that show that when a temperature difference is imposed between two reservoirs connected by Vycor rods in series with a chamber of solid helium, a pressure difference is induced between the two reservoirs that is described well by the thermo-mechanical (fountain) effect⁴⁶. In section IV, we show the results of experiments in which we use the fountain effect to induce flow through the solid. We describe the behavior of the flow at high temperature, and at low temperature where we observed an unexpected drop in the flux, followed by an increase in flux at the lowest temperatures we could reach with our apparatus (≈ 60 mK). In section V we discuss our results and offer comments. Finally, in section VI we summarize our results and present some further comments and conclusions.

II. CONCEPT AND DESIGN

The general design for the apparatus is similar to that used previously to search for D.C. flow through solid helium by mass injection^{32,33}. It exploits the properties of helium in confined geometries to allow for an inter-

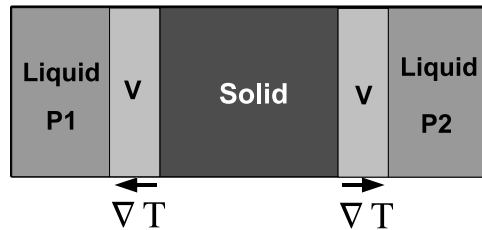


FIG. 1. Conceptual design of the flow experiments. Liquid-filled Vycor separates the solid from the two liquid reservoirs, and a temperature gradient across the Vycor allows the liquid reservoirs to remain in the bulk liquid region of the phase diagram, while the solid can be cooled to lower temperatures. The elevation of the melting pressure for the helium in the Vycor allows for an interface between the superfluid in the Vycor, and the bulk solid.

face between superfluid liquid and solid ^4He at pressures greater than the bulk melting pressure of solid helium. The concept of the experiment is shown in figure 1. It is known⁴⁷⁻⁴⁹ that the liquid-solid transition for helium in porous Vycor glass is elevated so that when the pressure of the helium in the Vycor is less than ≈ 35 bar, it remains a liquid. A chamber filled with solid ^4He is sandwiched between two liquid chambers with helium-filled Vycor separating the solid from the liquid. By imposing a temperature gradient across the Vycor, the outer chambers can be kept in the bulk liquid (superfluid) region of the phase diagram with the center chamber in the bulk solid region (figure 2). Thus an interface can exist between the superfluid liquid ^4He in the Vycor and the solid in the center chamber at pressures greater than the bulk melting pressure of solid helium (≈ 25 bar). In the absence of a porous material such as Vycor, the liquid-solid interface can only occur at the bulk freezing-melting pressure of the solid. Our design allows a chemical potential difference to be imposed across the solid with the Vycor acting as electrodes.

A schematic diagram of the cell used for these experiments is shown in figure 3. The solid helium is grown in region S, which has a cylindrical geometry, dia = 0.635 cm, (with side regions for access for future experiments), with a volume $V_{cell} = 1.84$ cm³. A capacitance strain gauge of the Straty and Adams type⁵⁰ (C1 and C2) is on each end of region S for *in situ* measurement of the pressure of the solid. Two Vycor rods, V1 and V2, enter region S through the top of the cell. The Vycor rods are 0.140 cm in diameter, 7.620 cm in length, and the cylindrical surface of the Vycor external to region S is sealed with a thin coating of Stycast 2850 FT epoxy. The Vycor penetrates into the cylindrical cell to about the mid-line axis of the cylinder. At the top of each Vycor rod is a liquid reservoir, R1 and R2; each reservoir is temperature-controlled with a heater, H1 and H2. The bottom of each Vycor rod has an epoxy patch across the

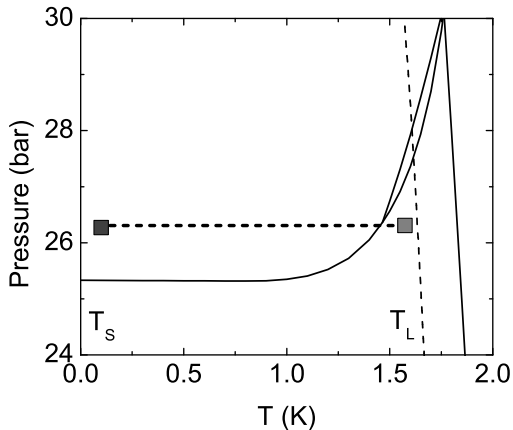


FIG. 2. Phase coordinates of the liquid reservoirs at temperature T_L and the solid at a typical temperature T_S and pressure where the experiments are preformed. The dashed horizontal line shows the temperature gradient along the Vycor. The dashed nearly vertical line represents the approximate location of the Lambda transition in helium-filled Vycor.

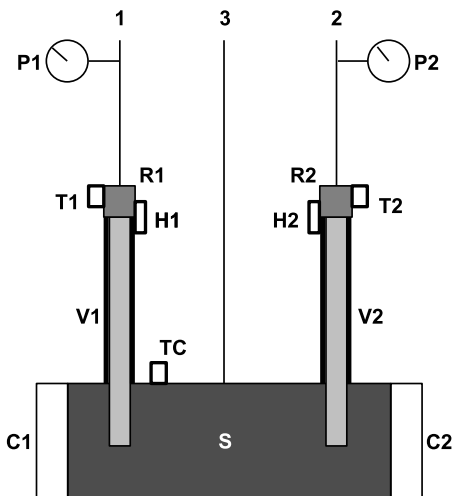


FIG. 3. Schematic diagram of the cell used for flow experiments. Three fill lines lead to the cell, capillaries 1 and 2 go to liquid reservoirs R1 and R2 above the Vycor Rods V1 and V2. The third fill line leads directly to the solid chamber, S. Two capacitance pressure gauges, C1 and C2, are located on either side of the cell for *in situ* pressure measurements. Pressures in the Vycor lines (1 and 2) are read by pressure transducers outside of the cryostat. Each reservoir has a heater, H1 and H2, which prevents the liquid in it from freezing, and the reservoir temperatures are read by calibrated carbon resistance thermometers T1 and T2. The cell temperature is recorded by a third calibrated carbon resistance thermometer, TC. The cell thermometer reading, denoted TC, measures the temperature of the sample, T.

end of the rod to ensure that an anomaly^{33,51} typically found along the axis of a Vycor rod is not an issue. Thus the cell is akin to a U-tube with solid at the bottom in chamber S, and superfluid on the sides in the Vycor and reservoirs.

The reservoirs are fed by stainless steel capillaries 1 and 2, which are heat sunk only at 4 K. To aid in the temperature control, each reservoir is thermally connected to the still of the dilution refrigerator, which is typically operated at $T \approx 800$ mK. The pressures in these lines, denoted as $P1$ and $P2$, are measured by pressure transducers located at room temperature. Another capillary, line 3, is used to fill the cell initially. This line is heat sunk at several places on the refrigerator, bypasses the Vycor rods and leads directly to region S. The cell is mounted on a copper plate which is attached to the mixing chamber of a dilution refrigerator by six copper rods of diameter 0.635 cm. The pressure gauges P1 and P2 are Paroscientific Digiquartz pressure transducers and the capacitive gauges C1 and C2 are monitored by an Andeen-Hagerling 2500-A capacitance bridge (C1) and by a General Radio 1615A bridge (C2), with a Stanford Research Systems SR830 lock-in amplifier. The reservoirs R1 and R2 shown in figure 3 represent the outer liquid chambers shown in figure 1. The heaters create the temperature gradient along the Vycor rods. Since capillaries 1 and 2 (which lead to the reservoirs) are heat sunk only at 4 K, no solid can form in them, and this provides a direct connection from the helium supply at room temperature to the reservoirs. With solid helium in region S, there is also solid helium in line 3, which prevents mass flow into or out of the cell through this capillary.

Mass flow in a superfluid system is governed by the chemical potential difference, $\Delta\mu$. If solid helium supports a superfluid flow, then flow should be induced by the imposition of $\Delta\mu$ between the Vycor rods. In the present context, for a superfluid $\Delta\mu = v\Delta P - s\Delta T$ where $v = V/N$ is the volume per particle and $s = S/N$ is entropy per particle. This implies that a flow can be induced by either a pressure difference^{32,33}, ΔP , or a temperature difference⁴⁵, ΔT . Previously we induced flow with the former. Here we focus on the latter. For such experiments, once a solid is present in the cell lines 1 and 2 are valved closed and line 3 is blocked by solid helium. By changing the thermal energy supplied to H1 and/or H2, we impose a temperature difference between the two reservoirs and monitor the flow between the two reservoirs by measuring the rate at which the pressure changes in the reservoirs, dP_i/dt where $i = 1, 2$ for the two pressure gauges.

The ^4He we use is ultra high purity ^4He with an assumed ^3He impurity concentration of ≈ 300 ppb; it was passed through a liquid nitrogen and a liquid helium trap. All of our samples are grown in region S, typically from the superfluid at constant temperature (for a more detailed discussion of this growth method, see ref. 52), but a few samples have been grown by the blocked capillary method³³. We note here that we have previously

discussed⁴⁵ the fact that growth above the melting curve from the superfluid has interesting temperature dependence, with such growth not possible for fresh samples below ≈ 300 mK. But, samples can be grown by this method above 300 mK, then be cooled and studied at lower temperature.

Once the solid is grown in the chamber, we can search for mass flow through the solid by changing the amount of thermal power deposited in the heaters H1 and H2. This procedure differs from the injection method^{32,33}, because after each measurement, the heater powers can be returned to their original settings, thus returning the system to the same initial conditions of temperature and pressure for the next measurement. In the injection method if the injection resulted in mass flow, the injection increased the pressure of the solid, and the subsequent measurement was then done at a higher pressure.

Our solid samples are identified by pairs of letters, assigned to the samples or to measurements of the samples in chronological order. So, for example, a sample might be created and labeled as GO and its pressure might be increased and the sample renamed as GP. Subsequent flow attempts at different temperatures on the same sample might be labeled GQ, GR, etc. By this means each measurement or manipulation of a sample is assigned a unique code. Tabulation of all solid samples discussed here is presented in the Appendix.

III. EQUILIBRIUM FOUNTAIN PRESSURE

If two containers of superfluid ^4He are connected by a superleak, a path through which only superfluid can flow, then a temperature difference imposed between the two containers will give rise to a pressure difference. This pressure difference, ΔP_f , known as the fountain pressure, is given by the fountain equation⁴⁶

$$\Delta P_f = \int_{T_a}^{T_b} \rho S dT. \quad (1)$$

Here $\Delta T = T_a - T_b$ is the temperature difference between the two containers, and ρ and S are the density and entropy of the liquid, respectively. When needed, values for $\rho(P, T)$ and $S(P, T)$ were taken from Maynard⁵³ and Donnelly⁵⁴ and extrapolated to above 25 bar where necessary.

With reference to figure 4 there are three fountain pressures to consider. One is due to the temperature difference between R1 and the cell, $\Delta T1 = T1 - TC$, another is due to the temperature difference between R2 and the cell, $\Delta T2 = T2 - TC$, and finally there is $\Delta TR = T1 - T2$, due to the temperature difference between R1 and R2. With superfluid present, $\Delta T1$ and $\Delta T2$ lead to separate pressure differences between the cell and the respective liquid reservoir, $\Delta P1$ or $\Delta P2$, given by equation 1, which are determined solely by the temperature of the respective reservoirs and TC . A non-zero value for

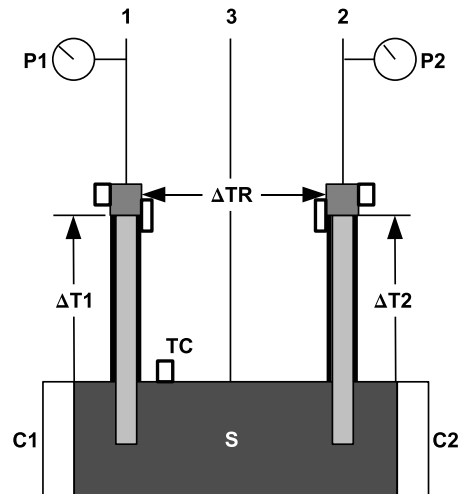


FIG. 4. Temperature gradients in the cell ($\Delta T1$, $\Delta T2$ and ΔTR), which lead to fountain pressures.

$T1 - T2$ results in a pressure difference between the two reservoirs, $\Delta PR = P1 - P2$, which can also be found using equation 1 with $T_a = T1$ and $T_b = T2$. If there is a supersolid that allows superflow in the cell, one may also think of ΔPR in a different way. In that case, one may think of the superfluid in R1 and R2 as connected by a superleak, $V1+S+V2$. With this perspective, we also have $\Delta PR = P1 - P2$.

A. equilibrium fountain pressure in liquid helium

Figure 5 shows the results of measurements that document the presence of the fountain effect when *liquid* ^4He fills chamber S at 65 mK near 20 bar. In figure 5a, $T2$ is held constant at 1.555 K while $T1$ is changed. First, $T1$ is raised in steps by increasing the thermal power deposited by H1. Each time $T1$ is raised, a rise in $P1$ is recorded with a corresponding drop in the cell pressure ($C1$ and $C2$) and $P2$. Next, when $T1$ is lowered by decreasing the thermal power deposited by H1, $P1$ is seen to drop, while $P2$, $C1$ and $C2$ all rise. When $T1$ is returned to its original value, all pressure values return to their original values; there is no hysteresis. Figure 5b shows the same type of measurement only this time $T1$ is held constant at 1.566 K and $T2$ is changed. Note that in figures 5a,b for relatively large values of $T1$ or $T2$ (e.g. $T2$ in figure 5b) the flow rate slows as the temperature of the reservoir is raised. This is likely due to a decreased superfluid fraction in the upper (warmer) region of the relevant Vycor rod. As will be described, during our flow measurements with solid in the sample cell changes in $T1$ or $T2$ were typically limited to ≈ 24 mK, as will be evident in figures presented later in this report.

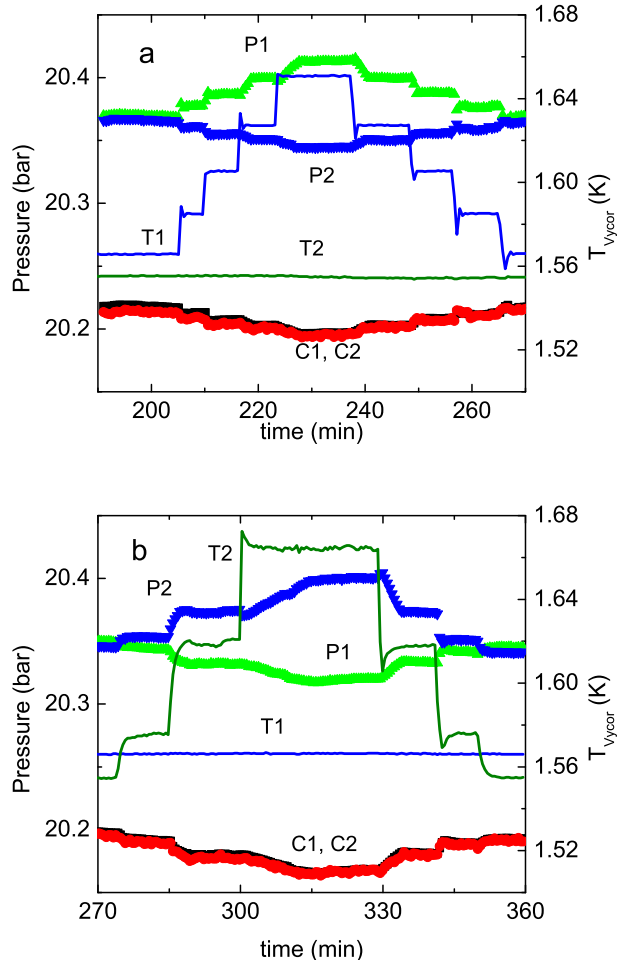


FIG. 5. (color online) Measurement of the fountain effect in liquid ^4He . Each increase in a reservoir temperature is accompanied by an increase in the pressure of the accompanying reservoir and a decrease in the pressure of the other reservoir. Decreasing the temperature reverses the process. (a) Changes in T_1 , (b) changes in T_2 . For these data $TC = 65$ mK. Transient effects in T_1 and T_2 associated with changes in temperature are due to the operation of the temperature regulators.

Figure 6 shows the measured pressure difference between each reservoir and the cell (where $C_1 = C_2$), $\Delta P_1 = P_1 - C_1$ and $\Delta P_2 = P_2 - C_2$, from the data in figure 5 along with the expected fountain pressure using equation 1 as described above. There is quantitative agreement between the two. Notice that in figure 6a $\Delta P_2 = \text{const.}$ and in 6b $\Delta P_1 = \text{const.}$ This constant behavior can be understood since the temperature difference between the respective reservoir and cell is constant, so the fountain pressure should not change. Thus, for example, as P_1 increases, P_2 and the cell pressure (measured *in situ* by C_1 and C_2) decrease together. Finally, figure 7 shows the pressure difference between the

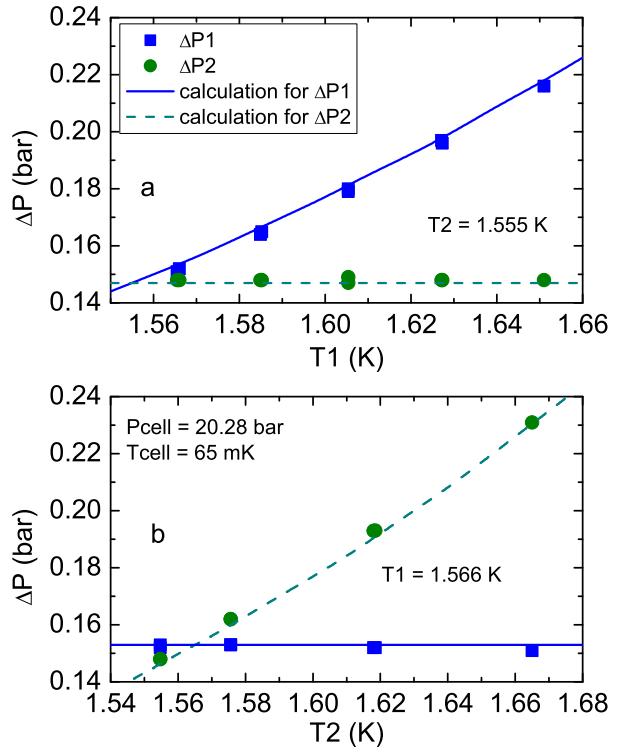


FIG. 6. (color online) Measured pressure difference between the reservoirs and the cell for (a) changes in T_1 with T_2 held constant, R1, $\Delta P_1 > 0$, and (b) changes in T_2 with T_1 held constant, R2, $\Delta P_2 > 0$, from the data shown in figure 5, along with the calculated fountain pressure from equation 1 for the same conditions.

two reservoirs, $\Delta PR = P_1 - P_2$, using the data shown in figure 5 along with the expected fountain pressure found from equation 1. Again, there is good agreement between the two meaning that the observed pressure differences observed with liquid ^4He in the cell are as expected from the fountain effect, equation 1.

B. equilibrium fountain pressure in the presence of solid

Figure 8 shows data from solid sample KE, grown from the superfluid at $TC = 352$ mK and then cooled to 100 mK. In a similar fashion to the liquid-only case shown in figure 5, T_1 was increased in steps and then subsequently decreased, while T_2 was held constant. Here, each increase in T_1 is accompanied by an increase in P_1 , (as shown for the liquid-only case in figure 5), and a decrease in P_2 and the cell pressures measured by C_1 and C_2 .

Although changes in $T_1 - T_2$ result in changes in P_1 and P_2 , figures 9a and 9b show that quantitatively the pressure differences induced, $\Delta P_i = P_i - C_i$ are not de-

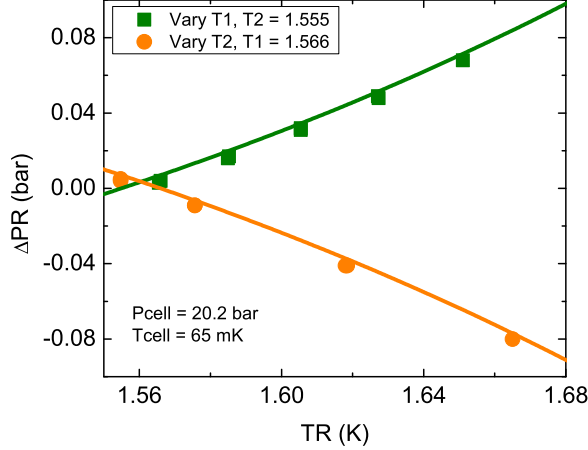


FIG. 7. (color online) Measured pressure difference between the two reservoirs, $\Delta PR = P1 - P2$, from the data shown in figure 5, along with the calculated fountain pressure for the same conditions. In each case TR is the temperature of the reservoir that is not held constant.

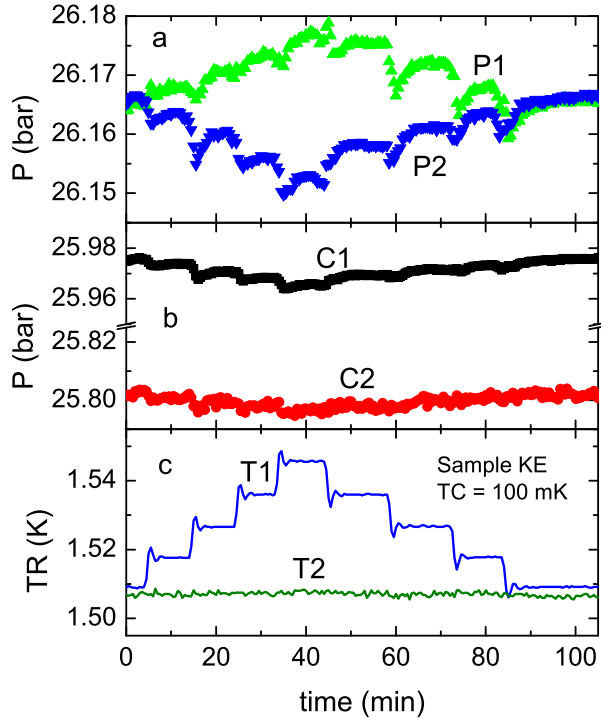


FIG. 8. (color online) Solid helium sample KE, $TC = 100$ mK. (a) Pressures, P1, P2, (b) Pressures C1, C2, (c) reservoir temperatures, T1, T2. T2 was held constant while T1 was changed in steps to measure the fountain pressures present. Typically the capacitor monitored with the General Radio bridge, here C2, showed a bit more noise.

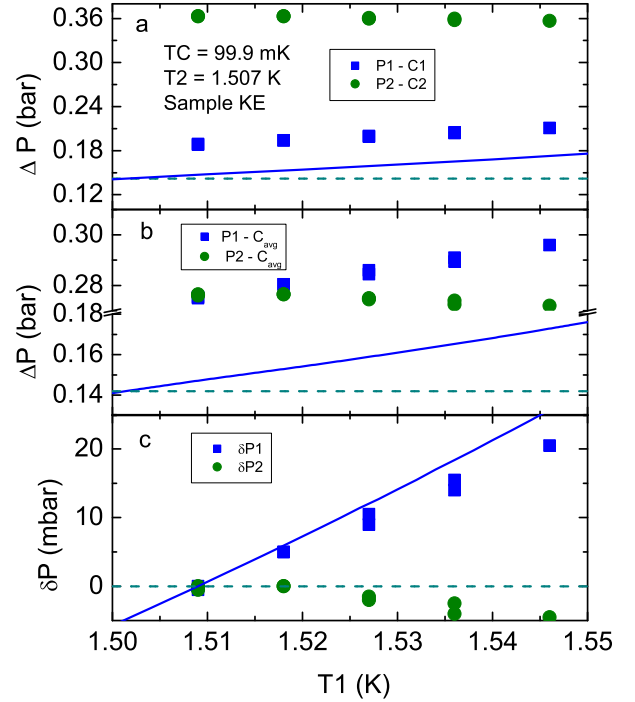


FIG. 9. (color online) Measurements of the pressure difference between each reservoir and the cell with solid in region S: sample KE, $TC = 100$ mK (figure 8). In each case the squares and circles refer to reservoirs R1 and R2, respectively, while the solid and dashed lines show predictions based on equation 1 for R1 and R2, respectively. (a) $P1 - C1$ and $P2 - C2$, (b) $P1 - C_{avg}$ and $P2 - C_{avg}$ where $C_{avg} = (C1 + C2)/2$ is the average between C1 and C2. Note the axis break. (c) $\delta P1$ and $\delta P2$ as defined in the text.

scribed by equation 1. This is not surprising. As we have noted previously^{33,52}, and as is evident in figure 8, there are often cases for which $\Delta C = C1 - C2 \neq 0$ when solid fills the cell. The presence of two separated *in situ* pressure gauges shows that the solid helium in our apparatus can sustain a stable pressure gradient; and, presumably the pressure can vary spatially in non-uniform ways throughout the solid. In fact, even with $C1 = C2$ with solid in the cell there is no reason to expect that the pressure difference $Pi - Ci$ can be predicted using 1. This is because the local pressure measured by each of the capacitors is not the relevant pressure to determine the fountain pressure. Figure 9 supports this. It shows $Pi - Ci$ (figure 9a) and $Pi - C_{ave}$ (figure 9b), where $C_{avg} = (C1 + C2)/2$ is the average between C1 and C2 from the data shown in figure 8, along with the predicted fountain pressure from equation 1. In this case, the data shows that the measured pressure difference differs from the predictions of equation 1.

We can look instead at the *change* in the fountain pressure that results from changing the temperature in the reservoir, $\delta Pi = \Delta Pi^j - \Delta Pi^0$. Here ΔPi^j represents the

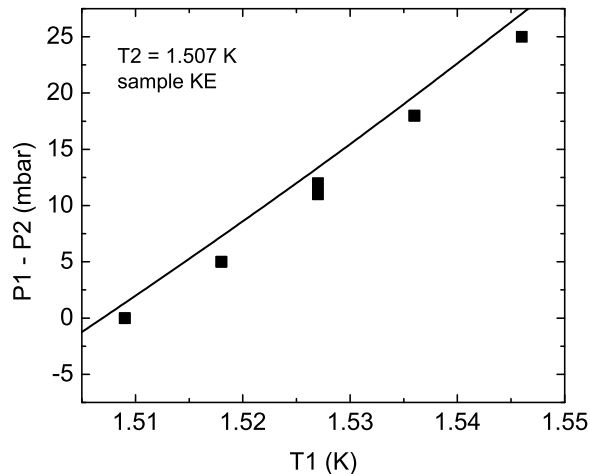


FIG. 10. Measurements of the pressure difference between the two reservoirs, $\Delta PR = P1 - P2$ with solid in region S: sample KE, $TC = 100$ mK (figure 8). The expected fountain pressure between the two reservoirs found from equation 1 is shown by the solid line.

difference between the pressure in reservoir, $i = 1, 2$, and the average pressure in the cell ($C_{avg} = (C1 + C2)/2$) after the j th temperature step. ΔP_i^0 is the pressure difference between the reservoir and the average of $C1$ and $C2$, when $T1 = T2$ (i.e. before the temperature step). Using this approach, δP_i^j was determined from the data shown in figure 8, and is plotted against $T1$ in figure 9c, along with the expected values calculated from equation 1. This tells us that *changes* in the cell pressure respond to *changes* in the imposed chemical potential in a predictable way. This behavior seems consistent with the presence of the climb of edge dislocations⁵⁵.

Figure 10 shows the equilibrium pressure difference between R1 and R2, ΔPR , determined from the data shown in figure 8 along with the expected pressure difference computed from equation 1. Here the data agree well with the fountain effect prediction. This shows that the presence of lattice pressure gradients in the solid has no effect on the equilibrium pressure difference between the two reservoirs, R1 and R2, caused by the fountain effect. The large pressure gradient in the solid seen in in the case of sample KE (figure 8) does not effect ΔPR . As long as there is mass flow present through the solid helium, any change in the temperature difference between the two reservoirs results in flow through the solid until the chemical potential equilibrates, regardless of any pressure gradients in the solid. Evidence for this is consistently present in the samples we have studied.

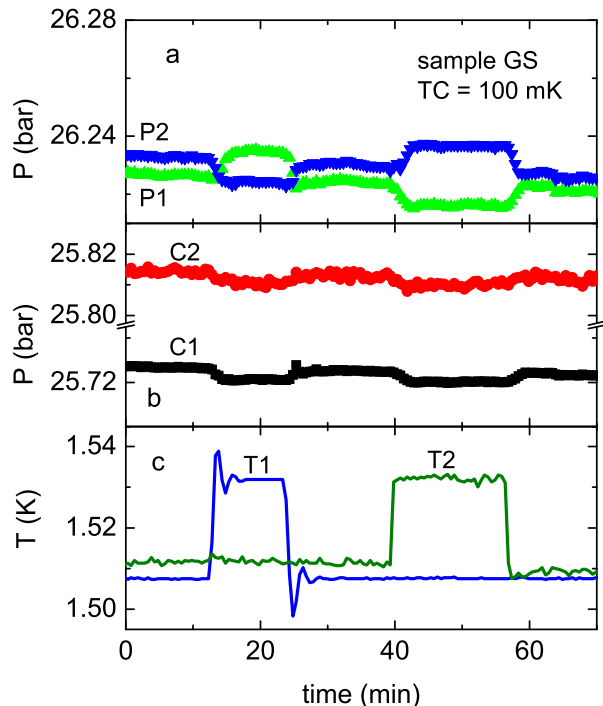


FIG. 11. (color online) Data that illustrates the procedure used to measure the flux through solid helium. (a) Pressures, $P1, P2$, (b) Pressures $C1, C2$, (c) reservoir temperatures, $T1, T2$. First $T1$ is raised by ≈ 24 mK. After equilibrium is achieved, $T1$ is lowered back to its original value, and the procedure is repeated with $T2$.

IV. MEASUREMENT OF MASS FLUX USING THE FOUNTAIN EFFECT

A. procedure

We next turn to the measurements of the flux induced through the solid when a temperature gradient is imposed between the two reservoirs. Figure 11 is an example of the procedure used to measure such flow; sample GS. This sample was grown from the superfluid at $TC = 317$ mK, cooled to 61 mK (sample GR), then warmed to 100 mK (sample GS, shown here). Starting with $T1 \approx T2$ ($T1$ is not always precisely equal to $T2$), $T1$ is raised by $\delta T1 = 24$ mK by increasing the thermal power supplied by H1 while $T2$ is held constant. $T1$ is held at this new temperature until after the new equilibrium is achieved after which $T1$ is returned to its original value. Next, after waiting for equilibrium, $T2$ is changed, with $T1$ held constant. For each change in temperature, the mass flux determined by dP/dt is measured to be constant in time with equilibration times of $dt_{eq} \approx 2 - 3$ min.

The constant (in time) nature of the flux following a change in the temperature in one of the reservoirs is more

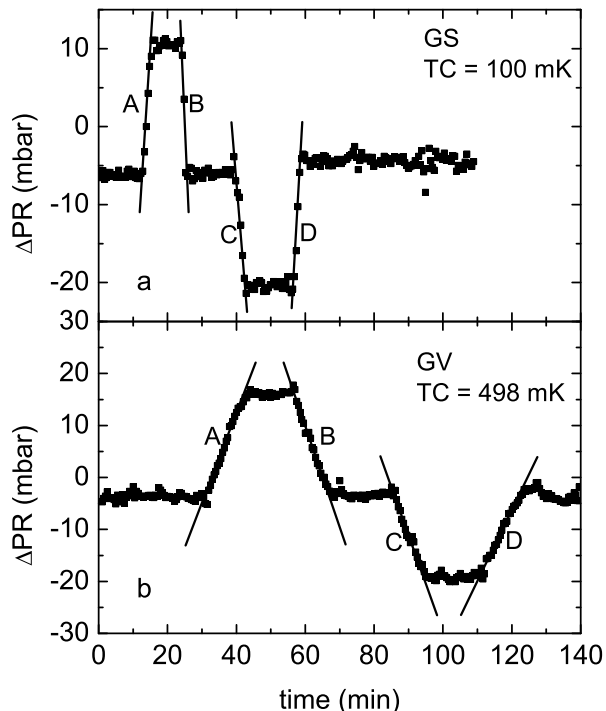


FIG. 12. $\Delta PR = P1 - P2$ for (a) sample GS at $TC = 100$ mK, (from figure 11), and (b) sample GV at $TC = 498$ mK. The non-zero baseline values of ΔPR result from small baseline differences between $T1$ and $T2$.

evident in figure 12, which shows the difference between the reservoir pressures $\Delta PR = P1 - P2$. ΔPR for sample GS ($TC = 100$ mK) is shown in figure 12a. For comparison we also show ΔPR for sample GV at $TC = 498$ mK in figure 12b. The flux for sample GV was much lower than for sample GS, with equilibrium occurring at $t \approx 15$ min. after changing the reservoir temperature.

A measured quantity proportional to the mass flux through the solid is the slope, $d(\Delta PR)/dt$, that results from changing the reservoir temperature. We label the slopes A, B, C and D so that, as shown in figure 12, slope A corresponds to the flux observed after increasing $T1$, and slope B corresponds to the slope that results from reducing $T1$ back to the original temperature. Likewise the slope labeled C gives a measure of the flux that results from increasing $T2$, while slope D results from reducing $T2$ back to the original temperature. With these definitions, there will be no ambiguity and all slopes will be reported here as positive numbers. Given the geometry of our apparatus, a typical value for $d(\Delta P)/dt$ with solid in our cell of ≈ 0.05 mbar/sec corresponds to a mass flux of $\approx 2.4 \times 10^{-8}$ g/sec, which is a flux of ≈ 3.6 cm³/year at the typical ⁴He density of these measurements. We report our flux values in the directly determined units, mbar/sec.

Using the procedure detailed above (figures 11 and 12)

the flux through solid helium can be measured at a series of temperatures. We grow a sample either from the superfluid at constant temperature or by the blocked capillary method. We then make flux measurements similar to those shown in figures 11 and 12, then change the temperature of the solid and repeat the measurement at the new temperature. As mentioned previously, this gives us measurements of the flux at different temperatures with the other parameters of the solid (i.e. base cell pressure) held constant (aside from modest pressure drifts occasionally seen).

B. flow in the range $100 \leq T \leq 700$ mK

The samples labeled GS (shown in figures 11 and 12) and GV (shown in figure 12) were part of a larger series of measurements, denoted as series sh03 (see Appendix). Here, the solid sample was grown from the superfluid at $TC = 317$ mK to a pressure of $C_{avg} = (C1 + C2)/2 = 25.8$ bar. The sample was then cooled to $TC = 61$ mK, and the flux was measured as detailed above (sample GR). The temperature was then raised to $TC = 100$ mK (sample GS), then sequentially to 698 mK (samples GT - GX) with the flux measured after each change in TC of ≈ 100 mK. The sample was then cooled back to 60 mK (samples GY - HE), again in ≈ 100 mK increments. Following the measurement at 60 mK the pressure of the solid was increased by a syringe injection⁵² (i.e. adding atoms through capillaries 1 and 2) to $C_{avg} = 26.0$ bar, and the temperature cycle was repeated (samples HG - HT, series sh04). More specific details will be provided in section IV D. In this section, we will focus on the data for the temperature range $TC \geq 100$ mK.

To characterize the flux and make comparisons among samples, we typically average the absolute value of all four slopes and define $d(\Delta P)/dt = ABCD = (|A| + |B| + |C| + |D|)/4$. Of course, there are other ways to represent the data, which will be discussed later, but here this will be useful and will allow us to bring forward points that we wish to emphasize. The results of such measurements of the flux found between 100 and 700 mK for the two series described above, series sh03 (samples GR - HE) and series sh04 (samples HG - HT) are shown in figure 13a along with measurements made in the liquid at a pressure of 24.3 bar. As the temperature is increased from 100 to 700 mK the flux with solid present drops smoothly, with $|d(\Delta P)/dt| = 0$ at $TC = 700$ mK. Upon cooling from this temperature, the flux is seen to rise, replicating the data taken while warming the solid. Note that series sh04, at a higher pressure, had slightly lower flux. This is consistent with our previous observations that have shown the flux to decrease with increasing pressure³³.

The liquid data shown in figure 13a represents a measure of the maximum average flux that the Vycor allows at 24.3 bar. It is seen to be relatively independent of temperature; a similar flux was measured at 22.1 bar. Comparing the flux through the solid to the flux through

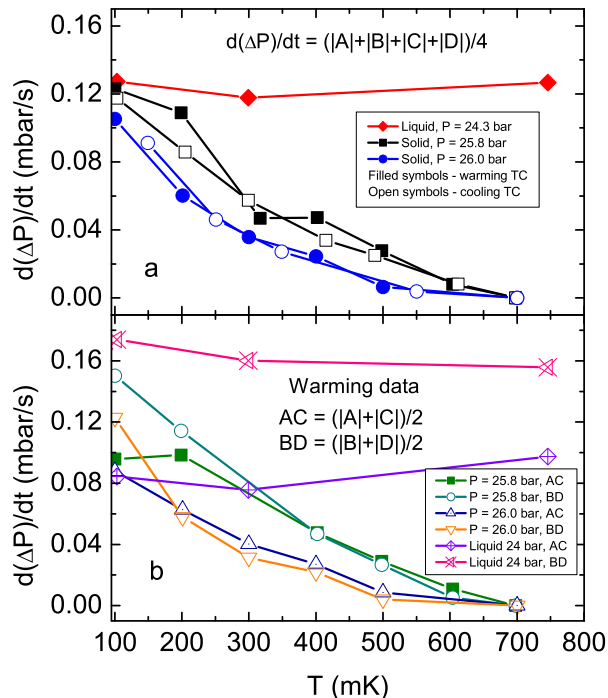


FIG. 13. (color online) Measured flux between 100 and 700 mK for series sh03 (25.8 bar), sh04 (26.0 bar), and liquid at 24.3 bar. (a) average of slopes A, B, C and D showing both warming and cooling TC. (b) average of A,C and B,D for warming TC only (see text). The liquid-only flux values are also shown. We take these to indicate that the Vycor may limit the flux, but only in the vicinity of 100 mK.

the liquid, it can be seen that at the higher temperatures, the flux through the Vycor with only liquid in the cell is considerably higher than the flux that is observed when solid is present in the cell. This suggests that the flux is most likely not limited by the flux through the Vycor in most of this temperature regime. As the temperature is lowered, the measured flux through the solid increases toward the measured flux through the Vycor with only liquid in the cell. At 100 mK, the two are close enough to each other, that we can no longer be sure that the solid is the bottleneck to the flux near 100 mK.

The possibility that the flux is limited by the Vycor instead of the solid near 100 mK is further demonstrated by figure 13b, which shows the averages of the warming slopes, $AC = (|A| + |C|)/2$, and separately the average of the cooling slopes, $BD = (|B| + |D|)/2$, for series sh03 and sh04 when increasing TC. At higher temperatures, that is $TC \geq 200$ mK, it is seen that $AC = BD$. But, as the temperature is lowered below 200 mK it is seen that $BD > AC$ meaning that the flux measured when cooling a reservoir is higher than when warming the reservoir for TC near 100 mK. This can be explained by assuming that near 100 mK the Vycor is limiting the flux because at higher reservoir temperatures ρ_s is reduced in the upper

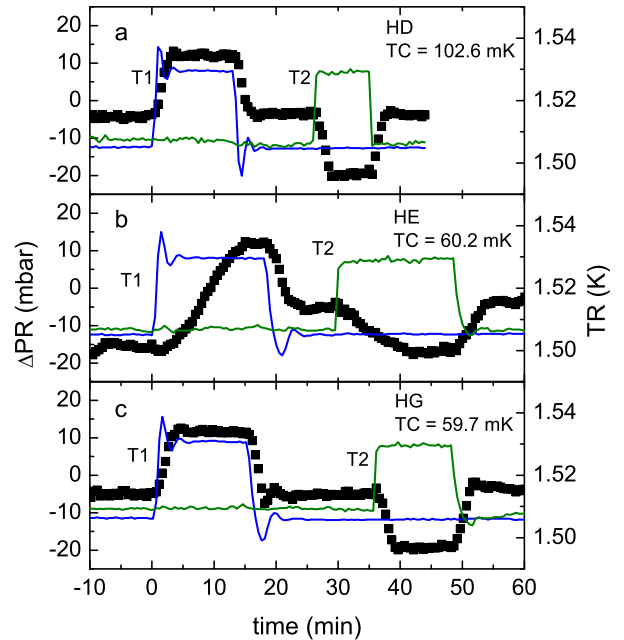


FIG. 14. (color online) Flux through samples (a) HD, (b) HE and (c) HG. The clock is reset for each data set so that $T1$ is increased at $t = 0$. In sample HE, which was cooled following the measurements on HD, there was much weaker coupling between the two reservoirs; the flux was much smaller. Following a ‘‘syringe injection’’ and a liquid helium transfer, sample HG showed a flux value similar to that seen for sample HD.

region of the Vycor rods (as is also seen in figure 5).

C. flow for $T \leq 100$ mK

Below 100 mK, some additional features are seen in the observed flux through the solid. First, recall that series sh03 was grown at $TC = 317$ mK, then cooled to 60 mK after which the flux was measured in 100 mK increments up to 700 mK, then cooled with the flux measured, following steps in TC of 100 mK. Near 100 mK (sample HD) the flux was consistent with earlier measurements (figure 14a). For example, for sample HD at 102.6 mK (figure 14a) the average of flow rate is $ABCD = 0.1175$ mbar/s. But, when the solid was returned to 60 mK (sample HE, figure 14b) a smaller and variable flow was seen between the two reservoirs. This weaker coupling is evident at the beginning of the measurement where $\Delta PR = -15$ mbar even though $T1 = T2$. Further, it is seen that the average flux is significantly smaller; for sample HE the flux is 0.0431 mbar/s, but the flow rate for each slope varies. At this point a helium transfer was needed. After filling the liquid helium bath, a ‘‘syringe injection’’⁵² added atoms to the cell to raise the pressure of the solid from 25.661 bar (sample HF) to 26.053 bar.

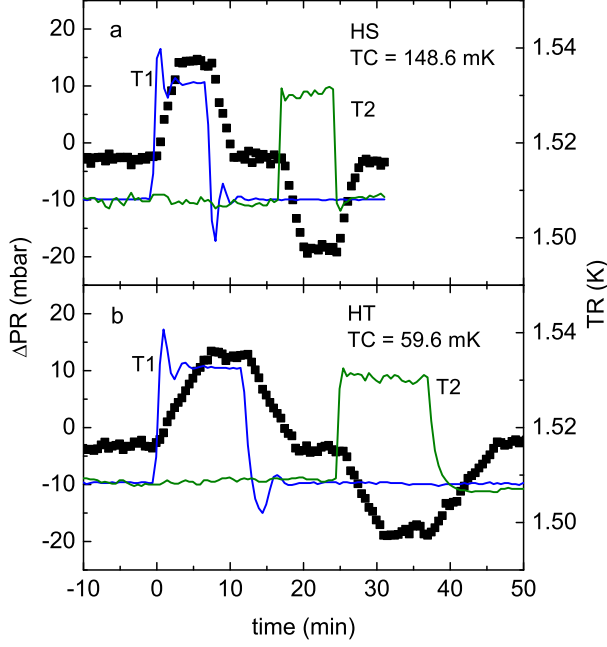


FIG. 15. (color online) Samples (a) HS at $TC = 148.6$ mK and (b) HT at $TC = 59.6$ mK. Both are part of the cooling data sets of series sh04. After cooling to 59.6 mK, the flux dropped similar to series sh03 (figure 14). Note that the time axis is shifted so that T1 is increased at $t = 0$ in each case.

At that point a fountain measurement revealed that a higher flux, $ABCD = 0.1067$ mbar/s had returned (sample HG) (figure 14c).

After repeating the temperature cycle at the higher pressure, $C_{avg} = 26.0$ bar (series sh04) the same observations were made, i.e. when returning the sample back to $TC = 59$ mK from above 100 mK, the flux dropped. Figure 15 shows the final two samples in this series, HS at $TC = 148.6$ mK, and HT at $TC = 59.6$ mK. Just as in the previous series, there is a significant drop in the flux as the temperature is lowered to 59.6 mK, but in this case the reduced flux was more stable.

Following measurement HT, a third sequence of measurements was performed with the same sample of solid helium in an effort to document this drop in the flux more closely. This was series sh04b, and is shown in figure 16a. Here, TC was warmed from 59 mK to 130 mK then cooled back to 60 mK with the flux measured at a stable temperature every 10 mK. Upon warming the solid there is a clear rise in the flux, which occurs near $TC = 80$ mK, and when cooling the sample, the flux drops near the same temperature. This change in the flux between fast flow and slow flow is seen to be rather abrupt, here seen to take place within the 10 mK change in cell temperature.

After series sh04b, the solid was melted, and a new sample of solid helium was grown from the superfluid at $TC = 317$ mK, then cooled to $TC = 100.8$ mK (sample

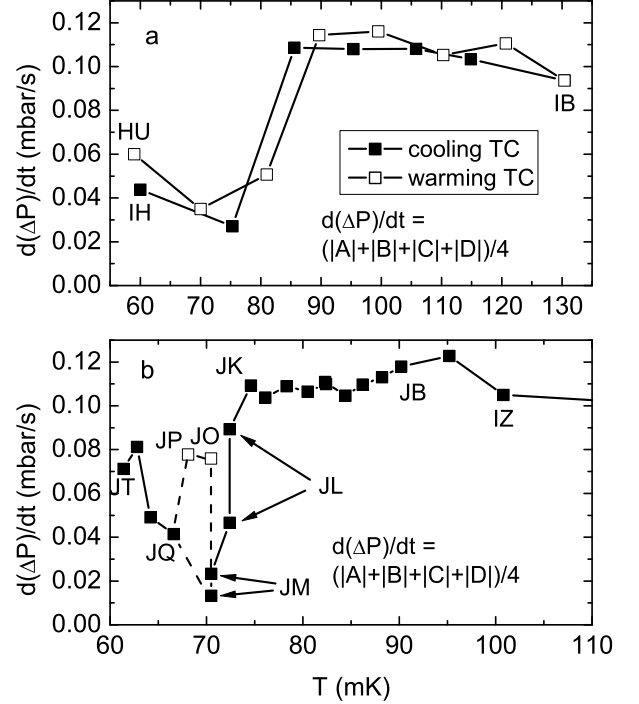


FIG. 16. (a) series sh04b in which the flux was measured starting at $TC \approx 60$ mK, then warmed in increments of 10 mK to 130 mK, then cooled back down in 10 mK increments to 60 mK. A change in the flux is seen to occur near $TC = 80$ mK. (b) series sh06b. Here the flux was measured in 2 mK steps as TC was lowered from 100 mK to 60 mK, and the flux dropped in the vicinity of $TC = 75$ mK. See text for a discussion of samples JO and JP.

IZ). The sample was then cooled further to $TC = 61.4$ mK with the flux measured every ≈ 2 mK; series sh06b, figure 16b. Here, the flux remained high until $TC \approx 75$ mK, then dropped to near 0 at ≈ 70 mK before rising again as the temperature was further lowered toward 60 mK.

In the vicinity of the flux minimum, dynamic behavior was observed. For example, following measurement JK at $TC = 74.6$ mK, the cell temperature was lowered to $TC = 72.5$ mK, and measurement JL was made, shown in figure 17a. Here the first step in T1 yielded slopes $A1 = 0.100$ mbar/s and $B1 = 0.154$ mbar/s. Then, the T2 step produced the slopes $C = 0.066$ mbar/s and $D \approx 0.034$ mbar/s, which is significantly lower than the flow rates measured in the T1 step (the D slope here is found by fitting to the steepest section). A subsequent second step in T1 produced the slopes $A2 = 0.030$ mbar/s and $B2 = 0.054$ mbar/s, which are similar to the C and D slopes. There was apparently some dynamic change in the solid that caused the slopes to change with time. These two different flow rates for sample JL are shown in figure 16b as $(|A1| + |B1| + |C| + |D|)/4$, and $(|A2| + |B2| + |C| + |D|)/4$.

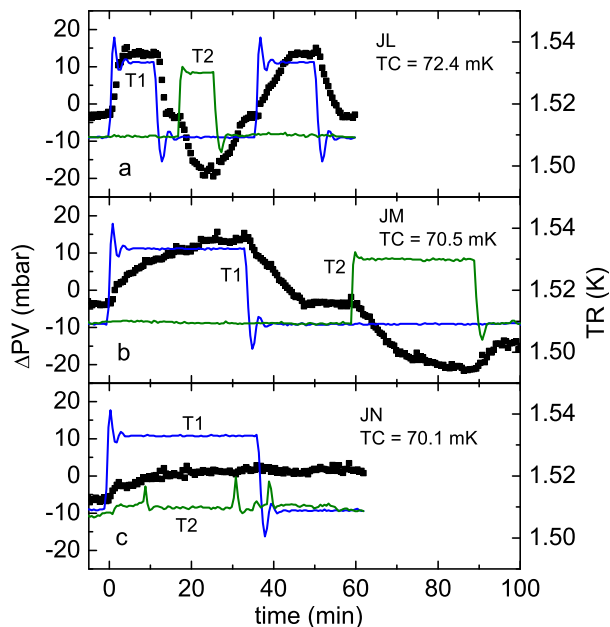


FIG. 17. (color online) Measurements (a) JL, (b) JM, and (c) JN. Successive measurements that show strong dynamic behavior. The time axis is shifted so that the increase in $T1$ occurs at $t = 0$ in each case.

Following sample JL, TC was lowered to 70.5 mK, and measurement JM was performed (figure 17b). The initial step in $T1$ produced a flow but no readily identifiable A slope, in fact, over the modest time span involved the flow data can be reasonably fit to an exponential relaxation with a time constant ≈ 13 min. Here, the A flux spans a range given by $A = 0.031$ to 0.008 mbar/s. We may also characterize the C-slopes by a range, $C = 0.022$ to 0.006 mbar/s. When $T2$ was subsequently returned to its original value, $|\Delta P|$ began to fall, but then stopped, and the data collection ended (the small bit of flow seen was used to determine the D slope for fig. 16b).

After 1.3 hours, another fountain measurement was attempted at $TC = 70.1$ mK (sample JN, fig. 17c). Here, an increase in $T1$ produced an initial change in $P1 - P2$, but only by 5 mbar. (Using equation 1, a 15 mbar pressure difference was expected). Additionally, when $T1$ was returned to its initial value, there was no change in $P1 - P2$ during an observation time of 35 min. JN is not shown in fig. 16b because there was time to change only $T1$ due to the need for a liquid helium transfer to the liquid helium bath. Near 70 mK there clearly seems to be dynamical behavior in the system that causes the flow rate through the solid to change with time and diminish to zero.

Following data set JN, the helium bath was filled (which introduces vibration), and the apparatus was left undisturbed for ≈ 16 hours before measurement JO, also done at $TC = 70.5$ mK, which is indicated by an open

square in fig. 16b. The average flux was $ABCD = 0.0755$ mbar/s, which is a marked increase from the previous few measurements. The next measurement, JP (the other open square in figure 16b), at $TC = 68.2$ mK showed a similar high flux, with $ABCD = 0.0773$ mbar/s. Then, as the sample was cooled further to 66.6 mK (sample JQ), the flow rate decreased again, before rising with decreasing temperature down to $TC = 61.4$ mK. Samples JO through JQ were all measured within ≈ 3.5 hours of each other (1.75 hours elapsed between the beginning of JO and the beginning of JP, while 1.6 hours elapsed between the beginning of JP and of JQ). We emphasize here that the variable flow rates seen deep in the flux valley have not been observed in other temperature regimes.

D. detailed behavior of one solid sample

It may be useful to follow the sequential evolution of the behavior of a single solid sample from its initial growth to the completion of its study, when it was melted. Before doing so, we first describe the creation and some manipulation of the solid sample. It was initially prepared by growth from the superfluid at 300 mK. Following growth, a syringe injection through lines 1 and 2 was done (we denote this as sample GP) at 317 mK to elevate the pressure to about 25.8 bar. A fountain measurement was then done (measurement GQ) at 317 mK, where the flux was found to be 0.0463 mbar/sec, a number shown in figure 13. The sample was cooled to 61 mK (measurement GR) and there followed a series of measurements (GR - HE) made while the cell temperature was increased and then decreased. Two of these measurements were at 60 mK. Measurement GR resulted in a flux of 0.1252 mbar/sec, but measurement HE resulted in a flux of 0.0431 mbar/sec. Measurement HE appeared anomalous. Its flux did not fit on the trend expected from the data shown in figure 13. A helium transfer was done and another syringe injection (which of course adds atoms to the sample and changes the sample pressure a bit) was done (sample HF), which resulted in a flux measurement HG (at $C_{avg} = 26.03$ bar at 59 mK) of 0.1067 mbar/sec.

Next, consider figure 18 where we show the sequential evolution of behavior of the single solid sample measurement from HG to the end of the sequence, IH (series sh04 and sh04b), at which point a transfer was needed and the sample was melted. This plot is absent two data points for which there were apparatus problems, but the evolution is clear. HG was warmed to 100 mK, a fountain measurement taken, and thereafter measurements were taken following 100 mK warming steps to 700 mK, (measurements HG-HN), a helium transfer was done, and the same sample was cooled to 550 mK and thereafter to 60 mK in steps of ≈ 100 mK (measurements HO-HT). Measurement HT resulted in a low value for the flux. At that point a transfer was done and the sample was measured at 59 mK (HU), where it showed a modestly higher flux,

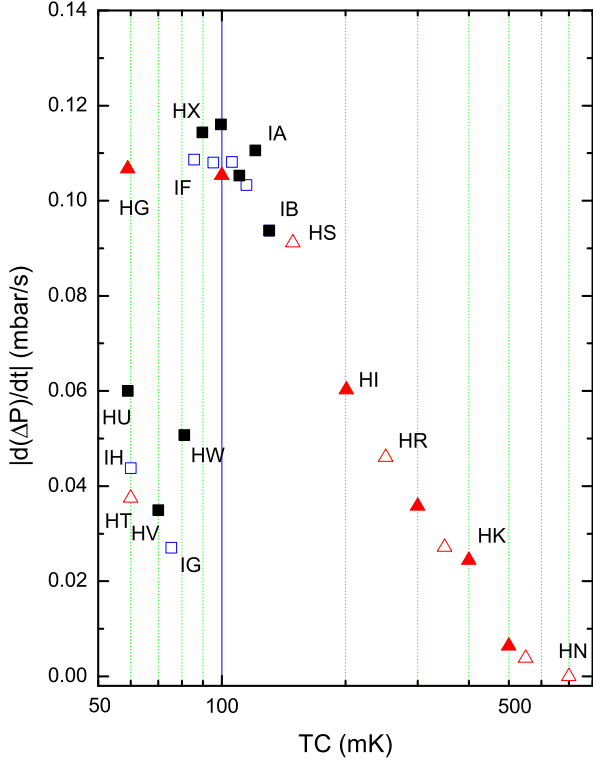


FIG. 18. (color online) Flux behavior of a single sample of solid. Beginning with sample HG (series sh04, sh04b), the temperature of the cell was changed to new stable values after which the flux was measured and after each change the same solid sample was given a new designation (see text and Appendix). Here $d(\Delta P)/dt = ABCD = (|A|+|B|+|C|+|D|)/4$. Samples HG-IH. Solid (open) symbols represent data taken while warming (cooling).

but still low. Then it was warmed in steps of 10 mK to 130 mK (measurements HV-IB), which caused the flux to pass through a minimum and a maximum and reproduce previous values of the flux in the higher temperature part of this range. The sample was then lowered in temperature to 60 mK (measurements IB-IH), passing through a flux minimum, at which point the sample was melted. The relatively robust nature of the temperature dependence of the flux for this single solid sample is demonstrated in figure 18.

Given the behavior of the flux below 100 mK seen in figures 16 and 18, it is important to ensure that this minimum in the flux is not due to some property of flow through the Vycor rods. Figure 19 shows data from series sh06b described previously and shown in figure 16b. Here, we separately plot the average flux found after warming each reservoir, $AC = (|A| + |C|)/2$, and after cooling each reservoir, $BD = (|B| + |D|)/2$, as also shown for $T \geq 100$ mK in (figure 13b). Above the flux minimum, $TC > 73$ mK, it is seen that $BD > AC$ meaning

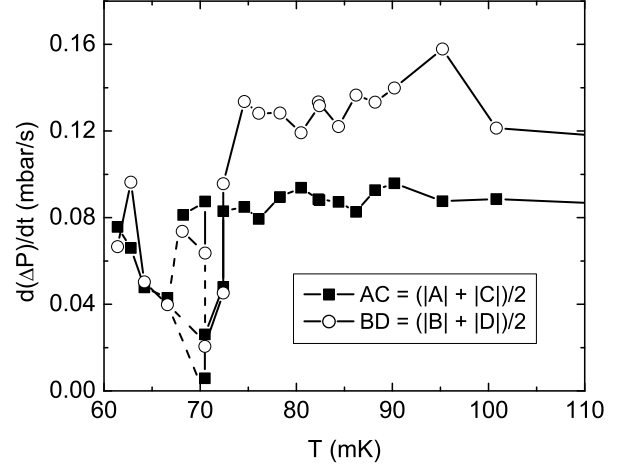


FIG. 19. The average of flow rates A and C (warming the reservoir temperature), and B and D (cooling the reservoir temperature) for series sh06b, described in section IV C.

that in *this* region ($75 \text{ mK} < TC < 110 \text{ mK}$), the Vycor is likely limiting the flow when a heater is on, just as was seen in figure 13b. However, in the vicinity of the flux minimum, it is seen that $AC \approx BD$ which indicates that the Vycor is not limiting the flow in this region, and that the flux minimum is due to some change in the flow paths in the solid chamber.

It should be noted that two solid helium samples did not show a drop in the flux near 75 mK. The first, series sh09, was grown from the superfluid at $TC = 320$ mK and cooled directly to 60.6 mK, then the flux was measured while warming the solid in ≈ 4 mK steps. No change in the flux was measured with $ABCD \approx 0.10$ mbar/s up to $TC = 91$ mK, the highest temperature studied in this sequence. Another series, sh11, involved a solid sample that was grown by the blocked capillary method and cooled to 63 mK and studied in the range 63 - 70 mK, which also did not show a drop in the flux. The sample temperature was raised to 300 mK and a syringe injection done to increase the pressure and the sample was returned to 61.2 mK, with a flux like that seen in the 63 - 70 mK range for samples in series sh09. This indicates that the flux minimum is likely sample-dependent and not caused by a simple thermal cycle of the solid.

V. DISCUSSION

It is not clear what the specific cause of the flux through solid helium is and in particular what is causing it to decrease and then rise at the lowest temperatures accessible to us. In samples that show the minimum in flux, it is quite robust. For instance, the minimum was observed in series sh03, sh04 and sh04b which were all with the same solid sample that had been thermally cy-

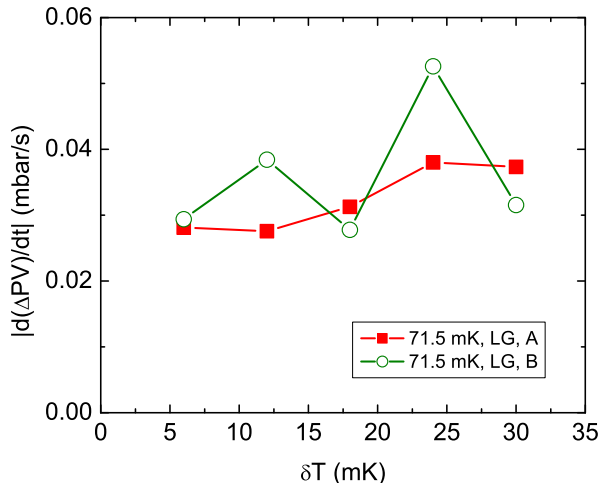


FIG. 20. (color online) The average of flow rates A (warming T1), and B (cooling T1) for measurement LG at $T_C = 71.5$ mK ($T_0 = 1.507$ K), in the region where the flux was seen to drop.

cled to 700 mK twice. In these series, the samples were also left overnight at 700 mK for ≈ 14 hours. Samples in series sh06, created at 317 mK and cooled to near 60 mK also showed the flux minimum. However, the fact that two other samples did not show this means that the presence of the flux minimum is not an intrinsic property of the solid; rather it must be related to the details of each particular solid, presumably due to the presence of some form of disorder.

A. nonlinearity

It has been suggested^{56,57} that the observed minimum in flux through the solid could be due to non-linear effects caused by the size of the chemical potential difference applied across the solid. If this is the case, when a sample is in the flux minimum different sized differences in the reservoir temperatures, $\delta T = T_1 - T_2$, are expected to produce different values for the flux. More specifically, smaller steps in the chemical potential are predicted to produce a higher flow rate.

To search for the possibility of these non-linear effects, different sized temperature differences, δT , were applied between the two reservoirs. For each δT , T1 was raised from a base temperature T_0 and held constant until equilibrium was established then returned to the original temperature (T2 was held constant the entire time). In this way, the A (warming) and B (cooling) slopes could both be determined for each size step. The results of these measurements are shown in figure 20, which shows the flow rate as a function of the temperature step for measurements of sample LG. Sample LG was grown from the

superfluid (at $T = 327$ mK), then cooled directly to 61 mK, then warmed to 71.5 mK where it was seen to be in a low flux state. Sample LG (because it was a low-flux sample) thus provides a test sample to search for non-linear effects in the flow due to the size of the chemical potential difference imposed across the solid. Sample KG (a high flux sample at 100 mK) provides a comparison (See appendix). For sample LG it is seen that slopes $A \approx B$, and there is no rise in the flux for smaller-sized temperature steps. So if there are non-linear effects in the solid causing the flow rate to decrease, then they must only diminish (and the flux rise) for temperature steps smaller than 6 mK.

B. possible roles of the ^3He impurity

Another possibility to consider in the context of the drop in the mass flux (e.g. at ~ 75 mK; figure 19) might be that it is due to the ^3He -induced pinning of dislocations. Pinning of dislocations is the mechanism that is thought to be responsible for the observed increase in the shear modulus with decreasing temperature first reported by Day and Beamish⁵, and the softening with increasing temperature seen by Rojas *et al.*²⁷. As the temperature is reduced, the dislocations become pinned either to each other, or to defects such as ^3He impurities, which makes the solid stiffer. If the dislocations provide the superfluid paths through solid helium, it is possible that the pinning can either enhance the effective conductivity of the pathways (pinning to each other) or reduce the flow of ^4He atoms through some of the superfluid cores (pinning by ^3He condensation on dislocation cores). Pinning by ^3He might be a cause for the drop in flux because the presence of ^3He on a dislocation might have an effect that would decrease the flux of ^4He along the dislocation core. And, if a mechanism were present that could enhance the interconnections in the dislocation network as the temperature is further reduced, this might provide bypass pathways around the blocking ^3He allowing a flux increase across the sample, while at the same time stiffening the sample.

We believe that it is unlikely that the drop in flux is in some (unknown) way related to bulk $^3\text{He} - ^4\text{He}$ phase separation. With the commercially available helium used in these experiments the concentration of ^3He is $x_3 \sim 300$ ppb. For this concentration the phase separation temperature is expected to be $T_{PS} = 51$ mK⁵⁸. It is not clear, however, if this is the actual concentration of ^3He in the solid. The cell is initially filled with helium from the third fill line, which bypasses the Vycor and preserves the ^3He concentration. The solid is most often grown above the melting curve by addition of ^4He through the Vycor rods, which presumably filters out the ^3He . This would tend to lower the x_3 in the solid, and lower the phase separation temperature. It is also possible that the ^3He in the cell diffuses to liquid regions, during solid growth⁵⁹, which may be present in the cell (perhaps including the Vycor,

which is filled with liquid). This would further lower x_3 in the solid and the phase separation temperature of 51 mK should be considered as an upper limit; $T_{PS} \lesssim 51$ mK. This makes it unlikely that phase separation is in any way associated with the observed low temperature drop in flux near 75 mK.

C. injection vs fountain measurements

Connections can be made between these flow experiments, and our previous flow experiments where a mass flow was induced by the injection method^{32,33}. In those experiments, flow was seen to cease for temperatures greater than ≈ 600 mK, which is similar to the observations noted here where no flow was seen for $TC > 650$ mK. Also, in both experiments, the mass flux is seen to be independent of the applied chemical potential gradient, which is consistent with superflow at a critical velocity.

There are also some differences between these results using the fountain effect to induce flow, and the previous injection experiments. Most notable is the absence of hysteresis when the temperature is thermally cycled using the fountain method. In the injection experiments, when a sample that showed mass flow was warmed to $T \gtrsim 600$ mK where it did not flow, it usually did not flow when cooled back to the original temperature (unless, once at that temperature the cell pressure was reduced slightly; then flow could be initiated). This behavior was not seen when using the fountain method. We note, however, that the procedure for the temperature cycles was somewhat different between the injection and fountain methods. In the injection methods, the sample was typically warmed in one step from low temperature (usually near 400 mK) to $T > 600$ mK, then returned with a temperature step of a similar size. In the fountain method, the sample was warmed in several smaller steps, but only to the temperature where flow was no longer observed, then cooled back down in steps.

Aside from slight differences in measurement protocol, the reason for the difference in behavior between the two methods used to induce flow may have to do with the fragility of helium crystals. It has been seen that in some temperature regimes solid helium crystals can be remarkably fragile, with non-linear effects occurring in strains^{5,59} as low $\sim 4 \times 10^{-8}$, which corresponds to a stress⁶⁰ of $\sim 8 \times 10^{-6}$ bar. The smallest pressure steps applied in the injection experiments was ~ 0.1 bar. This makes it very likely that each injection changes the solid in an irreversible way so that the next measurement has a different set of starting parameters. Using the fountain method, the pressure differences applied between R1 and R2 are typically $\sim 7 \times 10^{-3}$ bar. This is still a substantial pressure difference, but in this method the total mass in the system stays the same. By returning the Vycor temperatures back to their original values, each measurement can start with the same base pressure. We note here that whether by injection or by fountain techniques, when a

change in cell pressure is seen in C1, a similar change is seen in C2. This behavior is consistent with the climb of edge dislocations.

D. flow scenarios

Although as we have mentioned, it is not possible to make a definitive statement about what mechanism is at work to carry the flux we observe, it is useful to consider some of the possibilities that have been proposed. To do so in a quantitative way, we take a typical flux value of 0.06 mbar/sec, which corresponds to a typical mass flux (through the solid from one reservoir to the other) of 2.9×10^{-8} g/sec.

In the case of bulk flow we can write the mass flux as $dm/dt = \xi v \rho A$, where ξ represents the supersolid fraction, v the velocity, ρ the density, and A the cross sectional area that carries the flow. With a channel diameter of 0.64 cm, and a typical mass flux of $dm/dt = 2.9 \times 10^{-8}$ g/sec we find that $\xi v = 5.1 \times 10^{-7}$ cm/sec. So, if we take $\xi = 0.01$, then $v = 5.1 \times 10^{-5}$ cm/sec or 0.54μ /sec. On the other hand, if we take a velocity characteristic of that implied by some of the torsional oscillator experiments, $v = 10 \mu$ /sec, then we find, $\xi = 5.1 \times 10^{-5}$, which is smaller than the typical values deduced from torsional oscillator experiments, $\xi = 0.01\%$ to a few percent.

Edge dislocations have been suggested as a conduit that would allow superflux and also provide a mechanism for the increase in the density of the solid that is seen in our experiments. If we think in terms of an edge dislocation, the core of the dislocation will carry the flux. To be quantitative, we assume that the core of an edge dislocation has an effective cross sectional area of $A = 1$ nm². In that case, with $dm/dt = \xi v N \rho A = 2.9 \times 10^{-8}$ g/sec, where N is the number of edge dislocations that contribute to the flow, we find that $\xi v N = 1.7 \times 10^7$ cm/sec. If we take $\xi = 1$, and adopt a velocity of $v \leq 350$ m/sec (typical of a first sound velocity) as the maximum possible flow velocity, then $N \geq 480$, which suggests a dislocation density of ≥ 1600 cm⁻². For a smaller value of v there is a proportionate increase in N .

It was suggested previously⁶¹ that our flow results could be caused by liquid channels which have been shown to exist in solid helium samples on the melting curve³⁵. We have argued for various reasons^{33,37} that liquid channels are not likely the cause of our observed mass flux. The expected cross sectional area of a liquid channel³⁶ at 26 bar is ≈ 40 nm². Interpolating data^{48,62} gives a superfluid transition for this size channel of ≈ 1.55 K. This is inconsistent with our observations, which show that flow ceases at around 700 mK. None the less, we can apply a similar quantitative discussion and write that in the case of N_L liquid channels each of diameter $A \approx 40$ nm², the mass flux is given by $dm/dt = \xi v N_L \rho A$. So, with $dm/dt = 2.9 \times 10^{-8}$ g/sec we have $\xi v N_L = 4.3 \times 10^5$ cm/sec. If we take $\xi = 0.1$, then $v N = 4.3 \times 10^6$ cm/sec. If we make the assumption

that what limits the flow in such a channel is a critical velocity given by $v_c = K/2R$, where K is the circulation and $R = 7$ nm, then we find $v_c = 1.4 \times 10^3$. This then results in $N_L = 3070$ liquid channels. Although there are a number of assumptions, this strikes us as a rather large number.

Perhaps the most convincing argument that liquid channels are not relevant is the observation that if liquid channels were present, it is hard to understand how the flux for superfluid in such channels would decrease at lower temperatures (≈ 75 mK) and then increase again at even lower temperatures. So, we continue to believe that the evidence does not favor liquid channels as the conduction mechanism for the mass flux we measure.

E. comparisons to other work

The relation between these flow experiments, the torsional oscillator experiments and the shear modulus experiments remains unclear, although the dramatic changes in flux behavior that we measure take place near the temperature at which the torsional oscillator period and the shear modulus change rapidly with temperature. But, our experiments have shown the onset of flow to begin near $T \approx 600$ mK; the resonant period drop in the torsional oscillators (and rise in shear modulus) does not begin to change until 100-200 mK depending on the parameters of the sample, with the most dramatic changes seen near 70 mK for solid samples made with commercial ^4He .

One possibility is that the effects in the torsional oscillators at low temperatures are there at higher temperatures, but not visible at the frequencies at which the oscillators operate ($\sim 500 - 1000$ Hz); our present measurements are at essentially zero frequency. One might imagine that if dislocations are responsible, configurational changes might influence the tortuosity^{63,64}. Increases in tortuosity might make superfluidity be less visible at higher temperatures in torsional oscillator experiments, but this seems unlikely for a macroscopic dislocation density. If Reppy²⁵ is correct, the torsional oscillator period shift seen at low temperatures is not related to supersolidity. It may be that the presence of flow for $T > 80$ mK is due to different sample behavior than that which is causing the flow at lower temperatures. It is possible that the torsional oscillators observe the stiffening transition, while we see a true mass flux, a flux that is modified by the presence of the stiffening transition.

F. comment

The presence of dynamic behavior in the vicinity of the flux minimum causes us to offer a speculation. Perhaps it is possible that for $T \gtrsim 100$ mK many mobile dislocation lines can carry a net mass flux. For $T \lesssim 70$ mK a relatively stable network of cross linked dislocations may also

carry a net flux. But, in the vicinity of 75 mK by some mechanism there may be fluctuations in interconnection, which interrupt the effective flux in this crossover region, with perhaps a role for ^3He as noted earlier, and this results in the minimum. Perhaps this crossover region is what is seen in the specific heat measurements. In this scenario, the torsional oscillators and shear modulus experiments see a stiffening transition and the effects of flow are only seen in the experiments we have carried out, and perhaps the DC rotation experiments²⁸.

VI. SUMMARY

In section III we reported the observation of a thermo-mechanical (or fountain) pressure difference between two liquid reservoirs separated by hcp solid helium pierced by two spacially separated Vycor rods. This observation can be interpreted to mean that there is indeed a pathway (or pathways) for mass to flow through solid helium. Further, the constant flux, independent of pressure difference, through solid helium shown in section IV is indicative of a superflow at critical velocity, and so provides evidence that the paths are likely superfluid. Thus, taken as a whole, these two observations support the conclusion that superfluid-like behavior is present in a cell filled with solid ^4He . This superfluidity in solid helium is seen to appear at $T \approx 700$ mK, and the flux increases as the temperature is decreased until ≈ 100 mK. As the temperature is further lowered below 100 mK, the flux likely continues to rise (though we were limited in the maximum flux we could measure). This increase in the mass flux may signify an increasing superfluid fraction, ρ_s , in the conducting pathways or an increase in the effective number of conducting pathways.

It is still not clear what these pathways that allow for a superfluid connection through the solid are. Though much theoretical attention has been directed lately to the superfluidity of dislocations^{18,65}, there are other possibilities, such as flow through grain boundaries¹⁷ and flow through a glassy phase of solid helium¹⁹. Unfortunately, our apparatus cannot conclusively distinguish among these scenarios. But, the possibility of dislocations with dislocation interconnection dynamics and perhaps ^3He condensation, which seem consistent with the features we observe, appears to us to be the strongest possibility.

Near $TC = 75$ to 80 mK a sharp decrease in the flux is seen, with a subsequent rise the temperature is further lowered. It is not clear what causes this feature, but we have offered a possible scenario. It appears as though this drop is *not* an intrinsic property of the solid since some samples did not show a drop in the flux. We think it most likely that the flux minimum has something to do with the connectivity, ^3He condensation and the network of dislocations in the solid. We have not completely ruled out the presence of non-linearity that might be caused by the size of the applied temperature differences⁵⁶. Finally,

the flow rate is seen to rise again as the temperature is further lowered, which may be a sign of a switch in the mechanism that is causing the flow. Further study of this phenomenon to lower temperatures, higher pressures and different ^3He concentrations is necessary to fully understand what is causing it.

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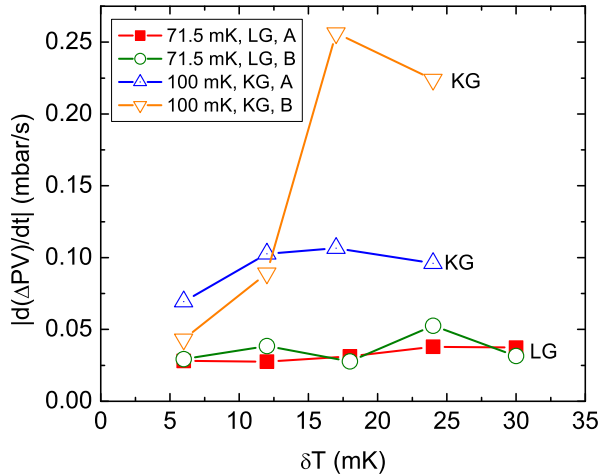


FIG. 21. (color online) The average of flow rates A (warming T1), and B (cooling T1) for measurement LG at $TC = 71.5$ mK ($T_0 = 1.507$ K), in the region where the flux was low, and for measurement KG at $TC = 100$ mK ($T_0 = 1.509$ K).

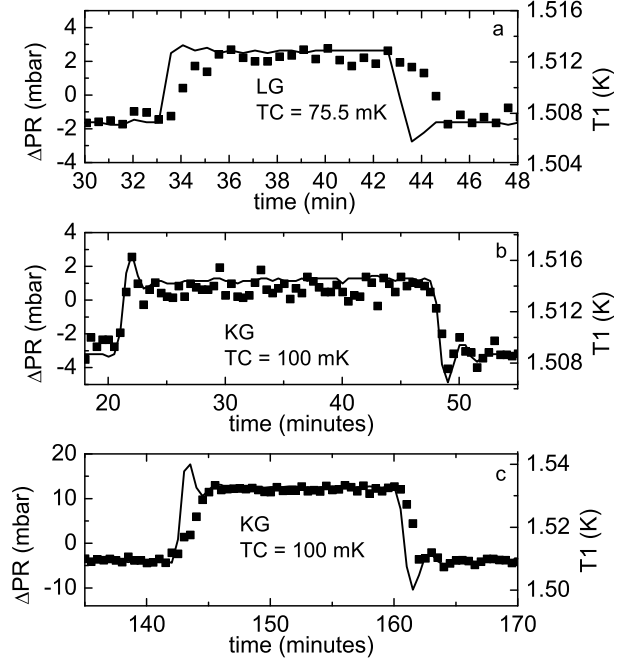


FIG. 22. (a) ΔPR for the 6 mK step in sample LG (b) ΔPR for the 6 mK step in sample KG, and (c) ΔPR for the 24 mK step in sample KG.

VIII. APPENDIX 1

In addition to the search for on-linear effects in a low flux sample (sample LG), we did a comparison study of a high flux sample, KG. Sample KG was a solid helium sample grown from the superfluid at $T = 352$ mK, then cooled to 100 mK where the different-sized temperature steps were applied. In sample KG for $\delta T \gtrsim 18$ mK it is seen that slope B > slope A, which is expected since the B slopes are measured at lower reservoir temperatures (figure 21). The apparent drop in the B slopes for sample KG for $\delta T \lesssim 12$ mK is likely due to the time constant associated with the reservoir's temperature controller, due to its design. For smaller applied δT the temperature controller changes the heater input at a slower rate, and since at 100 mK sample KG was in the high flux state, the flux is actually being limited by the rate at which the power delivered by the heater is increased in this small δT regime.

Figure 22 shows an expanded view of data measured with $\delta T = 6$ mK for samples LG (a) and KG (b), and $\delta T = 24$ mK for sample KG (c). (We note here that for all of the solid ^4He data we have presented prior to this point, through figure 19, $\delta T = 24$ mK.) Here it is seen that for the 6 mK step in KG (figure 22(b)) the time for the temperature to equilibrate, τ_T , is $\tau_T \approx \tau_P$, where τ_P is the time for the pressure equilibrate. In other words, the rate of change of the reservoir temperature is likely limiting the observed flow in the case of the 6 mK steps

in reservoir temperature for sample KG. On the other hand, it is seen that for the 6 mK step in LG (figure 22(a)), $\tau_T < \tau_P$, as is also the case for larger steps in sample KG, as shown in figure 22(c). This means that the discussion in section VA is correct, and in the low flux state no rise in the flux is seen at temperature steps as low as 6 mK (chemical potential difference = 4.8×10^{-10} J), i.e. non-linear effects are not observed. Further, if the minimum in the flux is due to non-linearities caused by the size of the temperature step (meaning that $\delta T < 6$ mK is needed), then this problem of equilibration times will make the effect very difficult to see in this apparatus as currently configured, since the situation will not improve as δT becomes smaller.

IX. APPENDIX 2

In this appendix we provide tables of flux values and base sample temperatures and pressures for many of the samples that are described in this report. In all of these tables, the temperature (TC) is in mK units, the pressures (C1, C2) are in bar units, and the flux values (AC, BD and ABCD) are in mbar/sec units. The units are not shown on the individual tables to improve the format. For the flux values, the designation AC means that the absolute values of the slopes of segments A and C

(measured following an increase of T1 (A) or T2 (C)) have been averaged. Similarly, the designation BD means that the absolute values of the slopes of segments B and D (measured following a decrease of T1 (B) or T2 (D)) have been averaged. ABCD designates an average of the absolute values of all four slopes. If a sample is missing from the alphabetical list, this signifies that (1) there was an instability of some sort in the data collection, which made the measurement unreliable or (2) the absence of a meaningful slope.

TABLE I. series sh03

sample	TC	C1	C2	AC	BD	ABCD
GR	61	25.723	25.829	0.0996	0.1508	0.1252
GS	100	25.724	25.815	0.0958	0.1502	0.1230
GT	199	25.706	25.800	0.1036	0.1142	0.1089
GU	402	25.717	25.840	0.0477	0.0469	0.0473
GV	498	25.720	25.865	0.0289	0.0267	0.0278
GW	604	25.746	25.927	0.0109	0.0052	0.0080
GX	698	25.720	25.930	0.0000	0.0000	0.0000
GY	612	25.718	25.909	0.0065	0.0098	0.0082
GZ	488	25.714	25.894	0.0222	0.0278	0.0250
HA	415	25.715	25.897	0.0375	0.0302	0.0338
HB	299	25.761	25.948	0.0533	0.0616	0.0574
HC	205	25.760	25.944	0.0850	0.0865	0.0858
HD	103	25.759	25.935	0.1101	0.1249	0.1175
HE	60	25.760	25.937	0.0207	0.0655	0.0431

TABLE II. series sh04

sample	TC	C1	C2	AC	BD	ABCD
HG	59	25.914	26.152	0.0980	0.1155	0.1067
HH	100	25.913	26.154	0.0880	0.1228	0.1054
HI	201	25.915	26.164	0.0626	0.0579	0.0603
HJ	300	25.917	26.174	0.0403	0.0313	0.0358
HK	400	25.931	26.202	0.0270	0.0219	0.0244
HL	500	25.885	26.126	0.0087	0.0041	0.0064
HN	700	25.892	26.120	0.0000	0.0000	0.0000
HO	550	25.960	26.224	0.0048	0.0029	0.0038
HQ	349	25.993	26.242	0.0279	0.0266	0.0272
HR	251	25.994	26.239	0.0466	0.0456	0.0461
HS	149	25.995	26.233	0.0922	0.0901	0.0912
HT	60	25.994	26.223	0.0405	0.0345	0.0375

TABLE III. series sh04b

sample	TC	C1	C2	AC	BD	ABCD
HU	59.0	25.939	26.150	0.0740	0.0461	0.0600
HV	70.9	25.942	26.154	0.0346	0.0353	0.0350
HW	81.9	25.944	26.157	0.0388	0.0627	0.0507
HX	89.7	25.947	26.163	0.0876	0.1413	0.1144
HY	99.5	25.949	26.166	0.1076	0.1246	0.1161
HZ	110.3	25.952	26.172	0.0952	0.1154	0.1053
IA	120.7	25.953	26.174	0.1093	0.1119	0.1106
IB	130.4	25.953	26.174	0.0898	0.0976	0.0937
IC	114.9	25.953	26.174	0.0918	0.1148	0.1033
ID	105.8	25.976	26.203	0.0875	0.1288	0.1081
IE	95.4	25.977	26.205	0.0945	0.1216	0.1081
IF	85.6	25.978	26.206	0.0884	0.1290	0.1087
IG	75.3	25.985	26.213	0.0306	0.0235	0.0271
IH	60.0	25.993	26.224	0.0469	0.0407	0.0438

TABLE IV. sh06b

sample	TC	C1	C2	AC	BD	ABCD
IY	326	26.021	26.019	0.0463	0.0453	0.0458
IZ	100.8	26.002	25.979	0.0887	0.1214	0.1050
JA	95.2	25.998	25.974	0.0876	0.1579	0.1228
JB	90.2	26.000	25.976	0.0959	0.1399	0.1179
JC	88.2	26.004	25.981	0.0928	0.1333	0.11302
JD	86.2	26.009	25.986	0.0827	0.1367	0.1097
JE	84.4	26.012	25.991	0.0873	0.1221	0.1047
JF	82.3	26.016	25.996	0.0885	0.1334	0.1110
JG	82.4	26.054	26.030	0.0881	0.1317	0.1099
JH	80.5	26.056	26.040	0.0939	0.1192	0.1065
JI	78.3	26.057	26.040	0.0896	0.1283	0.1089
JJ	76.1	26.056	26.039	0.0795	0.1282	0.1038
JK	74.6	26.057	26.047	0.0849	0.1337	0.1093
JL	72.4	26.058	26.050	0.0480	0.0453	0.0466
JM	70.5	26.059	26.051	0.0135	0.0206	0.0171
JO	70.5	26.040	26.108	0.0871	0.0638	0.0755
JP	68.2	26.039	26.108	0.0811	0.0735	0.0773
JQ	66.6	26.041	26.112	0.0430	0.0399	0.0414
JR	64.2	26.042	26.113	0.0478	0.0504	0.0491
JS	62.8	26.220	26.466	0.0661	0.0964	0.0812
JT	61.4	26.200	26.437	0.0757	0.0666	0.0712

TABLE V. series sh09

sample	TC	C1	C2	AC	BD	ABCD
KO	60.6	25.986	25.936	0.0807	0.1168	0.0987
KP	62.2	26.158	26.078	0.0857	0.1179	0.1018
KQ	66.0	26.178	26.091	0.0837	0.1142	0.0990
KR	69.6	26.195	26.104	0.0846	0.1146	0.0996
KS	75.3	26.156	26.102	0.0842	0.1115	0.0978
KU	80.5	26.196	26.133	0.0745	0.1440	0.1092
KV	85.5	26.214	26.146	0.0872	0.1648	0.1260
KW	91.0	26.133	26.084	0.1088	0.2026	0.1557

TABLE VI. series sh11

sample	TC	C1	C2	AC	BD	ABCD
KZ	61.2	25.825	25.814	0.0927	0.1464	0.1195
LA	64.7	25.769	25.783	0.0988	0.1579	0.1283
LB	69.0	25.759	25.775	0.1106	0.2077	0.1591
LD	61.2	25.868	25.906	0.1067	0.1511	0.1289
LE	64.5	25.876	25.909	0.0911	0.1755	0.1333

TABLE VII. series sh12

sample	TC	C1	C2	AC	BD	ABCD
LF ^a	26.095	26.044	61.2	0.0471	0.0498	0.0485
LG ^a	26.103	26.055	75.5	0.0380	0.0561	0.0470
LH	81.9	26.139	26.088	0.0484	0.0415	0.0449
LI	84.7	26.141	26.109	0.0934	0.1662	0.1298
LJ	91.6	26.309	26.261	0.0806	0.1805	0.1305
LK ^a	26.389	26.332	94.7	0.1289	0.1588	0.1439

^a Only A and B slopes were used.